

Next Generation of Multifunctional Polymeric Membranes for Resource Recovery

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Outline

- Background
- Overview and Summary of Recent Advances
- Acknowledgments



Separation Science and Technology (SST) as a Convergence Platform for *SusChEM*, *Sustainable Chemistry, Engineering and Materials*

Separation Science and Technology (SST) for a Sustainable Energy, Water and Materials Nexus



Separation S&T Platform

Separation Processes Separation Materials Separation Systems

Integral Element

Reclaiming and Maintaining The Environment

Membrane Technology for a Sustainable Energy, Water and Materials Nexus

- Polymeric membranes are critical for a broad range of sustainability related applications including
 - Energy conversion and storage
 - Water treatment, reuse and desalination
 - Gas separations
 - Biofuel processing
 - Metal and resource recovery
 - **Biochemical separations and purifications**

Current Polymeric Membranes

- Current commercial polymeric membranes perform a single function such as
 - Salt rejection in desalination using a dense and composite membrane
 - Particle rejection in algae separations and harvesting using a porous and low-pressure membrane
 - Proton transfer in fuel cells by a cation-exchange membrane



Multifunctional Polymeric Membranes

- Membrane technology is moving towards advanced membranes that perform multiple functions with improved flux and fouling resistance including:
 - Solute rejection
 - Sorption
 - Catalysis
 - Charge transport

Next Generation Polymeric Membranes: Mixed Matrix Membranes With Emebbeded Nanomaterials

- Convergence of membrane technology and nanotechnology to prepare mixed matrix and composite membranes with embedded nanomaterials
 - Carbon nanotubes
 - Graphene
 - Zeolites
 - Metal oxide nanoparticles
 - Metal organic frameworks
 - Dendritic macromolecules (Our Group)
 - Polymeric nanoparticles (Our Group)

MMMs With In-Situ Generated Polyethyleneimine (PEI) Particles as Weak-Base Membrane Absorbers



SEM Images of MMMs With In-Situ Generated PEI Particles



Kotte, M. R., Cho, M. and Diallo, M. S. A Facile Route to the Preparation of Mixed Matrix Polyvinylidene Fluoride Membranes with *In-Situ* Generated Polyethyleneimine Particles. *J. Mem. Sci.* **2014**, 450, 93-102.

Composition of MMMs With In-Situ Generated Polyethyleneimine (PEI) Particles

Membrane Composition	NSM-1		NSM-2		NSM-3		PVDF (Neat)	
••••• F ••••••	Wt,g	Wt, %	Wt, g	Wt, %	Wt, g	Wt, %	Wt, g	Wt, %
PVDF	5.25	73.32	5.25	62.16	5.25	52.27	5.25	100
[a] PEI Particles	1.91	26.68	3.196	37.84	4.794	47.73		

FTIR Spectra of the Control PVDF and With In-Situ Generated PEI Particles



New IR Peaks from PEI particles:

- 1. NH₂ bending (1635 cm⁻¹)
- 2. NH Stretching (3255 cm⁻¹)
- 3. OH stretching (3410 cm⁻¹)

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XPS Spectra of the Control PVDF and Mixed Matrix Membranes



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Surface Compositions of MMMs With *In-Situ* **Generated PEI Particles As Determined by XPS**

Membrane Sample	Concentration (wt%)				
	С	F	0	Ν	
PVDF	51.71	48.29			
NSM-1	53.93	38.2	6.85	1.02	
NSM-2	54.46	36.01	8.25	1.28	
NSM-3	57.37	28.41	12.38	1.84	

Contact Angles of MMMs With In-Situ Generated PEI Particles



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Zeta Potentials of MMMs With In-Situ Generated PEI Particles



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Water Permeability of the NSM-2 Membrane With In-Situ Generated PEI Particles



Water permeability of the NSM-2 membrane is equal to ~23 Liters/m²/hr/bar.

Water permeability of an ultrafiltration (UF) membrane typically varies from 50 to 800 Liters/m²/hr/bar.

NSM-2 membrane behaves as a "tight" UF membrane

Protein Binding Experiments: Protocol

The NSM-2 membrane was employed in these experiments

Run 1: Pure water (Compaction)	Run 2: Pure water flux (run)				
Feed: DI water; pH: 6.0	Feed: DI water; pH: 6.0				
Pressure: 1 Bar	Pressure: 1 Bar				
Compaction: 30 min	Run time: 60 min				
Run 3: BSA solution (run)	Run 4: DI water wash (cleaning)				
Concentration: 1000 mg/L	Membrane cleaning in DI water under stirring Cleaning time: 60 min				
pH: 6.50					
Run time: 60 min					
Pressure: 1 Bar					
Run 5: Pure water flux (post cleaning run)					
Feed: DI water					
pH: 6.0					
Pressure: 1 Bar					
Run time: 60 min					

Protein Binding Experiments: Results

The NSM-2 membrane was employed in these experiments



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MMMs With In-Situ Generated PEI Particles as Weak-Base Membrane Absorbers

BSA: Bovine Serum Albumin Protein (1000 mg/L)



Other Reported Preparation Routes for Weak-Base Membrane Absorbers

Surface-initiated atom transfer radical polymerization



BSA binding capacity: 96 mg of protein per mL of membrane in PBS buffer (pH ~7)

Qian et al. Appl. Surf. Sci. 271, 2013, 176–183

Our Approach for Preparing Weak-Base Membrane Absorbers: One Pot Synthesis

No surface-initiated atom transfer radical polymerization is needed



Our Approach for Preparing Weak-Base Membrane Absorbers: In-Situ Synthesis of PEI Particles in the Casting Solutions

No prior synthesis of the PEI particles by inversion suspension polymerization is needed

Suspension crosslinking





Bulk crosslinking ♪



Diallo, MS and co-workers Branched polymeric media: perchlorate-selective resins from hyperbranched polyethyleneimine. *Environ. Sci. Technol.* **2012**. 46:10718-10726.

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