

# Liquid Hydrogen: Safety and Design Considerations

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# About Tom

- ▶ 38 years of experience with GH2 and LH2 systems
- ▶ Managed Air Projects NA Gases Engineering Group
- ▶ Managed hydrogen transfill
- ▶ Developed global hydrogen processes, equipment, and procedures with large hydrogen supplier.
- ▶ H2 codes and standards Member for Compressed Gas Association (CGA) and National Fire Protection Association (NFPA)
- ▶ Involved in numerous hydrogen hazard system reviews
- ▶ Member of the Hydrogen Safety Panel

**Thomas Witte, PE**  
**Chemical Engineer**

**Witte Engineered Gases**



# About Harold

- ▶ PhD in Chemistry
- ▶ NASA for over 30 years
- ▶ NASA Safety Standard for Hydrogen Systems
- ▶ NASA Hydrogen Safety Training Instructor
- ▶ WHA International Since 2019
- ▶ Hydrogen Design and Safety Training
- ▶ Hydrogen Risk Analysis
- ▶ Failure investigation
- ▶ Member Hydrogen Safety Panel
- ▶ Member CHS
- ▶ Member ISO TC 197
- ▶ Husband to Margie, 3 daughters and 13 Grandchildren



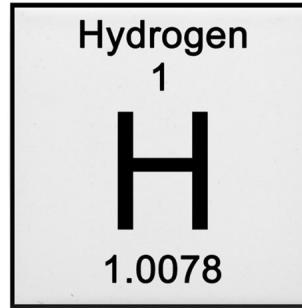
# Topics to be covered by Harold

- ▶ Hydrogen properties
- ▶ Fire and explosion hazards
- ▶ Materials
- ▶ Liquid hydrogen hazards
- ▶ Liquid hydrogen spill procedures
- ▶ Training

# Hydrogen (H<sub>2</sub>) Properties

## ► Gaseous Hydrogen (GH<sub>2</sub>)

- Fuel (i.e. flammable gas)
- Colorless, odorless, tasteless gas
- Non-corrosive, non-toxic
- Simple asphyxiant
- Lightest gas



## ► Liquid Hydrogen (LH<sub>2</sub>)

- Non-corrosive liquid fuel (i.e. flammable)
- Cryogenic liquid at -423 °F (-252.8 °C | 20.3 K)
- Burn hazard if contact with skin
- At boiling temperature, all gases except He are solid
- ~800 times more dense than GH<sub>2</sub> and 14x less dense than water
- 1 vol. liquid expands to 848 vol. gas (23x more than water)



Image from [wiki/Liquid\\_Hydrogen](https://en.wikipedia.org/wiki/Liquid_Hydrogen)

# The Problem

When hydrogen mixes with an oxidizer...

...the risk of ignition is high

Unique Molecular Properties



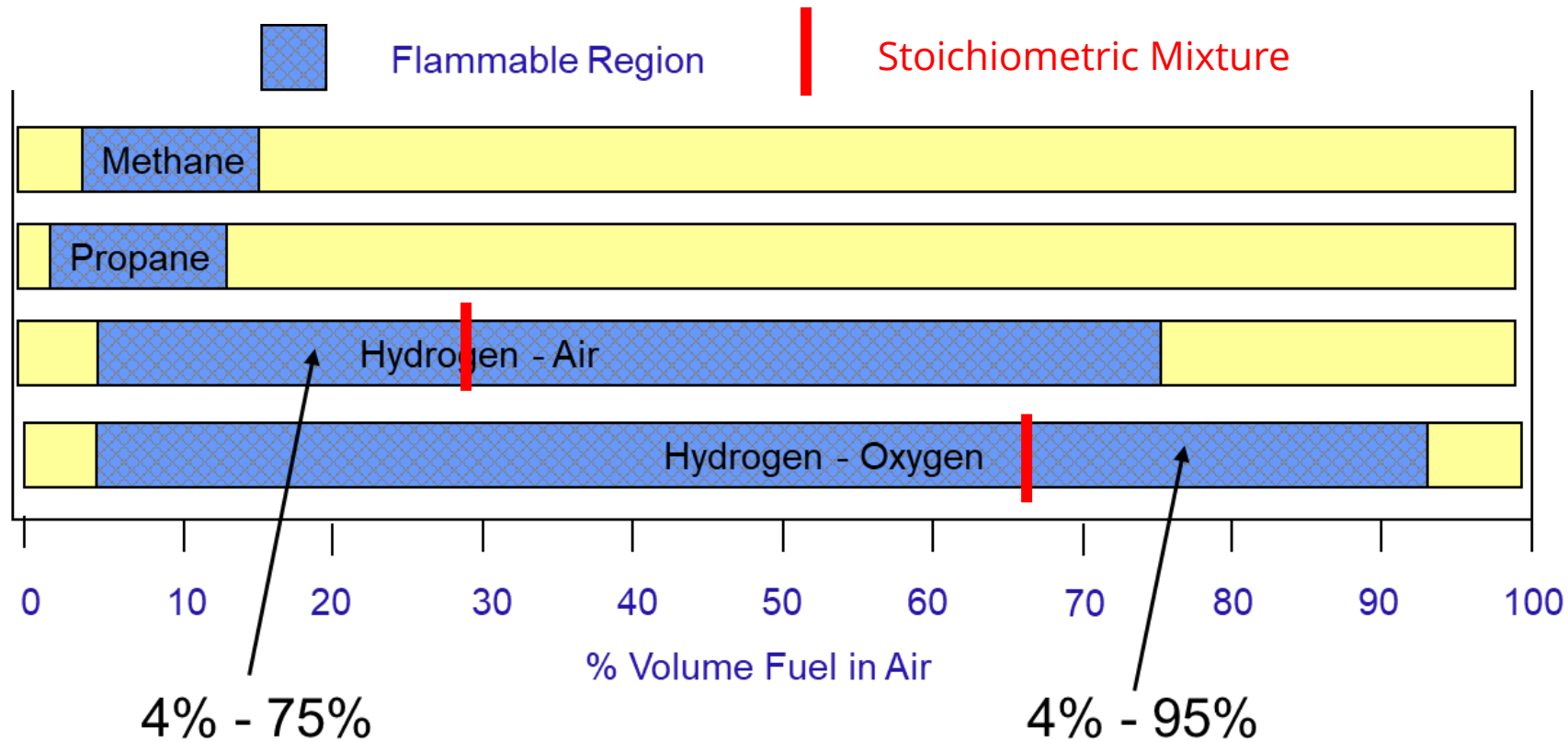
Low Ignition Energy

oxidizer

Wide Flammability Range

# In Comparison to Other Flammable Gases

At ambient pressure and temperature



# In Comparison...

<b>Min. Ignition Energy in Air @ 1 ATM</b>	<b>0.017 mJ (1.6x10<sup>-8</sup> BTU)</b>
<b>Min. Ignition Energy in Oxygen @ 1 ATM</b>	<b>0.0012 mJ (1.1x10<sup>-9</sup> BTU)</b>

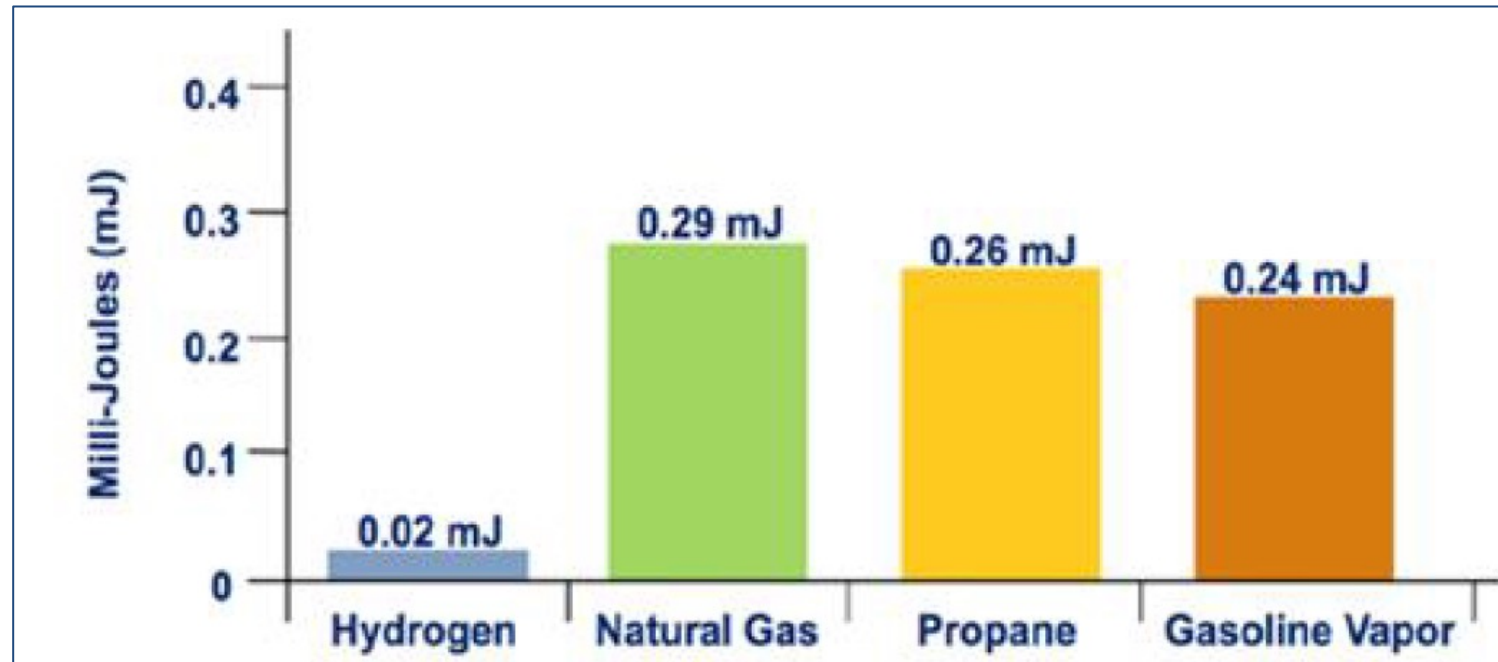


Image from H2Tools Hydrogen Compared to Other Fuels  
<https://h2tools.org/bestpractices/hydrogen-compared-other-fuels>



# Ignition Mechanism Statistics

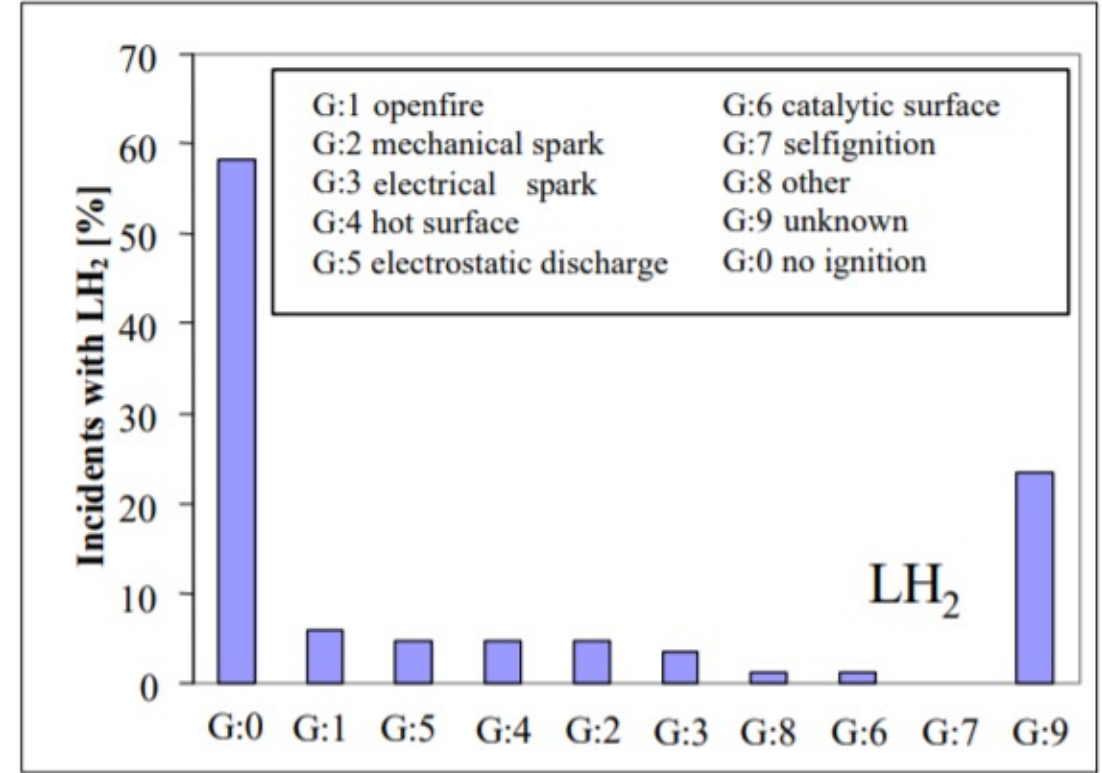
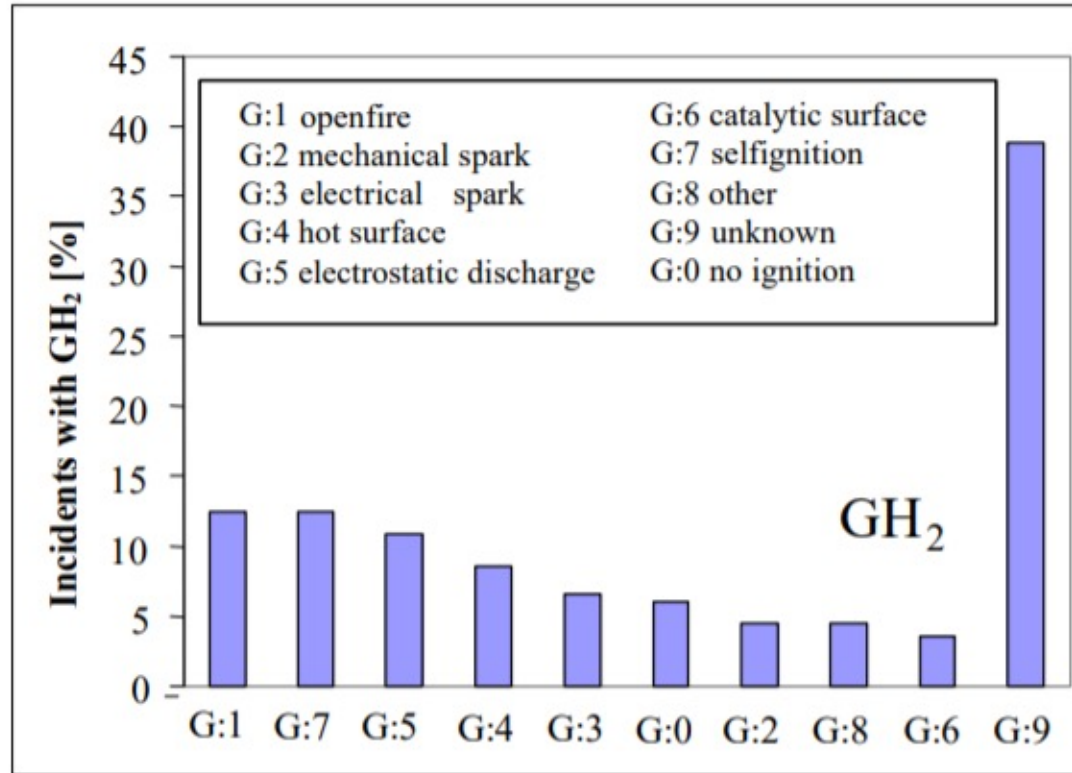


Image from: W. Breitung, Analysis Methodology for Hydrogen Behavior in Accident Scenarios 2016  
Original data from: Kreiser et al. 1994

# NIST H<sub>2</sub> Release in Garage

## H<sub>2</sub> Concentration Near Ceiling

16%



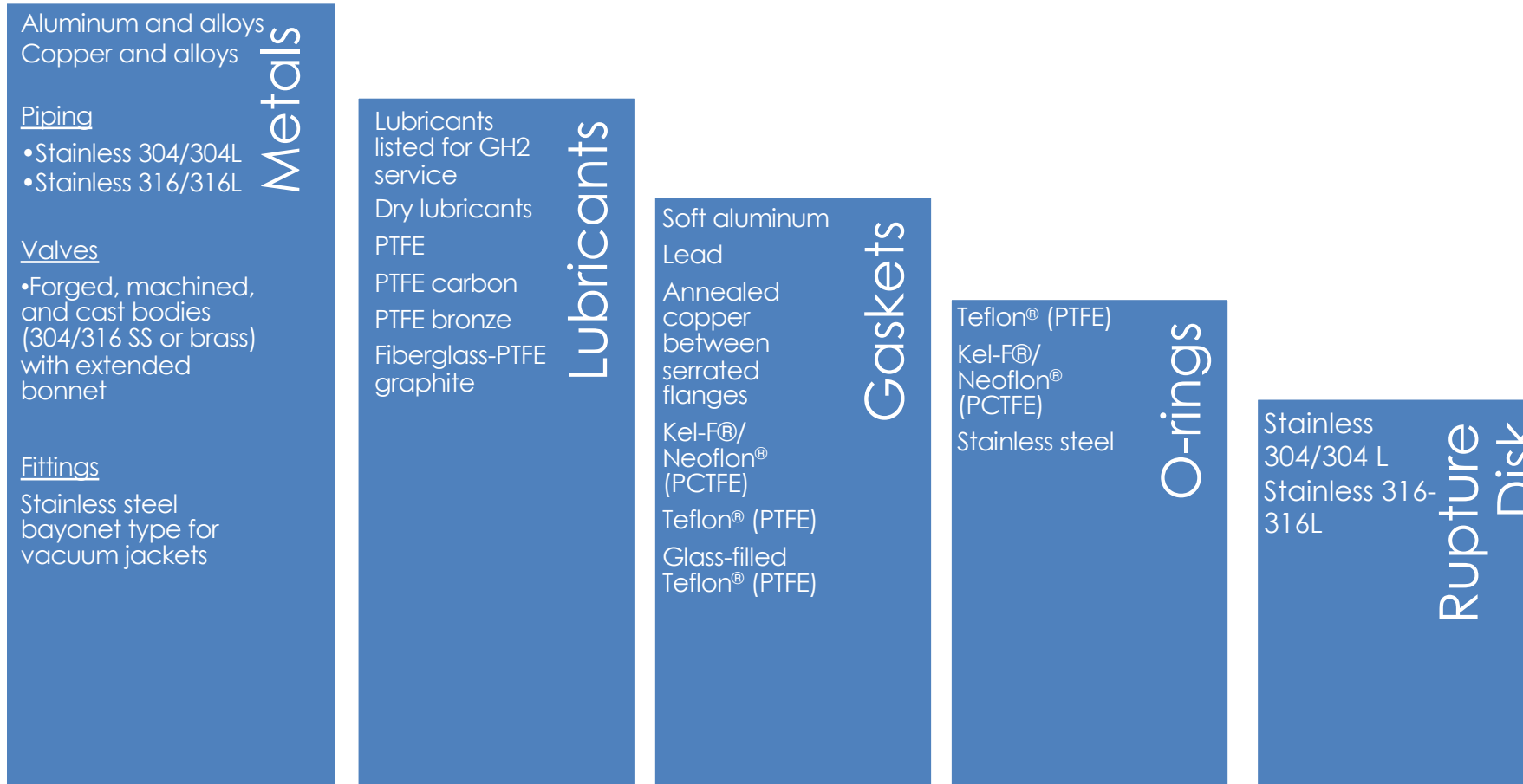
- Concentration @ 15in: ~10%
- Burn down to 15 in. height
- Peak temp: 444 °C
- Deflagration speed: 7-10 m/s

28.8%



- Concentration @ 15 in: ~23%
- Deflagration speed: 25 m/s
- Debris field extended 46 m (150 ft)

# Examples of Preferred Materials List for LH<sub>2</sub>



# LH<sub>2</sub> Hazards

- ▶ At boiling temperature of LH<sub>2</sub>, all gases except He become solid
  - Leaks can plug flow restrictions and/or be explosion hazards
- ▶ LH<sub>2</sub> has one of the highest expansion ratios of any cryogen
  - 1 vol. Liquid → 848 vol. gas
  - Continuous venting required to prevent overpressure



# Liquid Lockup



Video from Linde North America Training Course: Taking the Lead in Safety – Working with Hydrogen

- ▶ Although LH<sub>2</sub> vessels are designed to keep the liquid cold, boil off is inevitable
- ▶ Clear vent paths are important!
  - Trapped hydrogen will vaporize when warmed and generate overpressures in equipment if not vented
- ▶ Vent valves should not be open when not in use
  - Air intrusion may freeze, blocking relief
- ▶ Un-insulated piping, liquid, or cold vapor presents a burn risk to personnel
- ▶ System must be designed to be able to purge air and moisture
  - Use He as the inert gas

# LH<sub>2</sub> Personal Protective Equipment

## No exposure to liquid is expected

- Safety glasses
- Leather gloves
- Fire resistant clothing with long sleeves
- High-top leather boots

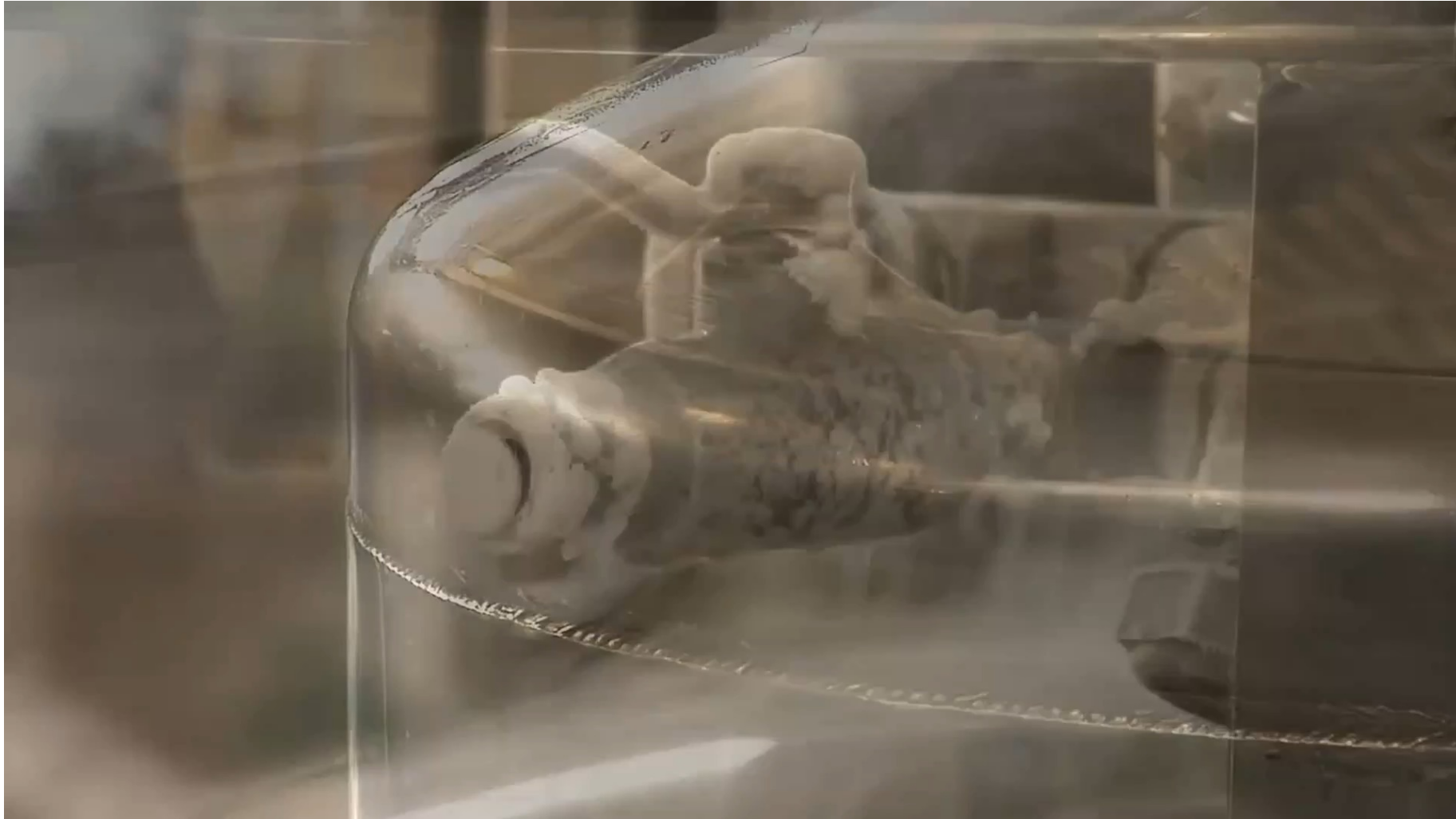
## Possibility of liquid exposure

### ADD:

- Face shield
- Insulated gloves



# Low Temperature Results in Liquid Air Forming



Video from Linde North America Training Course: Taking the Lead in Safety – Working with Hydrogen



# LH2 Leak / Spill Procedures

- ▶ LH<sub>2</sub> will rapidly boil or flash to a gas if exposed to ambient temperatures
- ▶ Leaks and spills will appear as fog clouds
  - Presents burn, asphyxiation, fire and/or explosion hazards
  - If possible, shut off H<sub>2</sub> source
  - Evacuate area until liquid has evaporated and gas has dispersed below LFL
  - Be aware that the cold, dense H<sub>2</sub> gas formed can remain close to the ground

# LH<sub>2</sub> Plume Dispersion Study

White Sands Test Facility, New Mexico

4 mph (6.4 km/h) wind



14 mph (22.5 km/h) wind



# Training

- ▶ Training is critical for safe operation, maintenance, and emergency response.
- ▶ Include in training
  - Operations
  - Maintenance personnel
  - Site operators and personnel
  - Emergency responders is
- ▶ Training in proper maintenance procedures, including purging techniques, to assure air/hydrogen mixtures are minimized is key.
- ▶ Procedures should be planned and not developed at the final moment



# Available Training Center for Hydrogen Safety

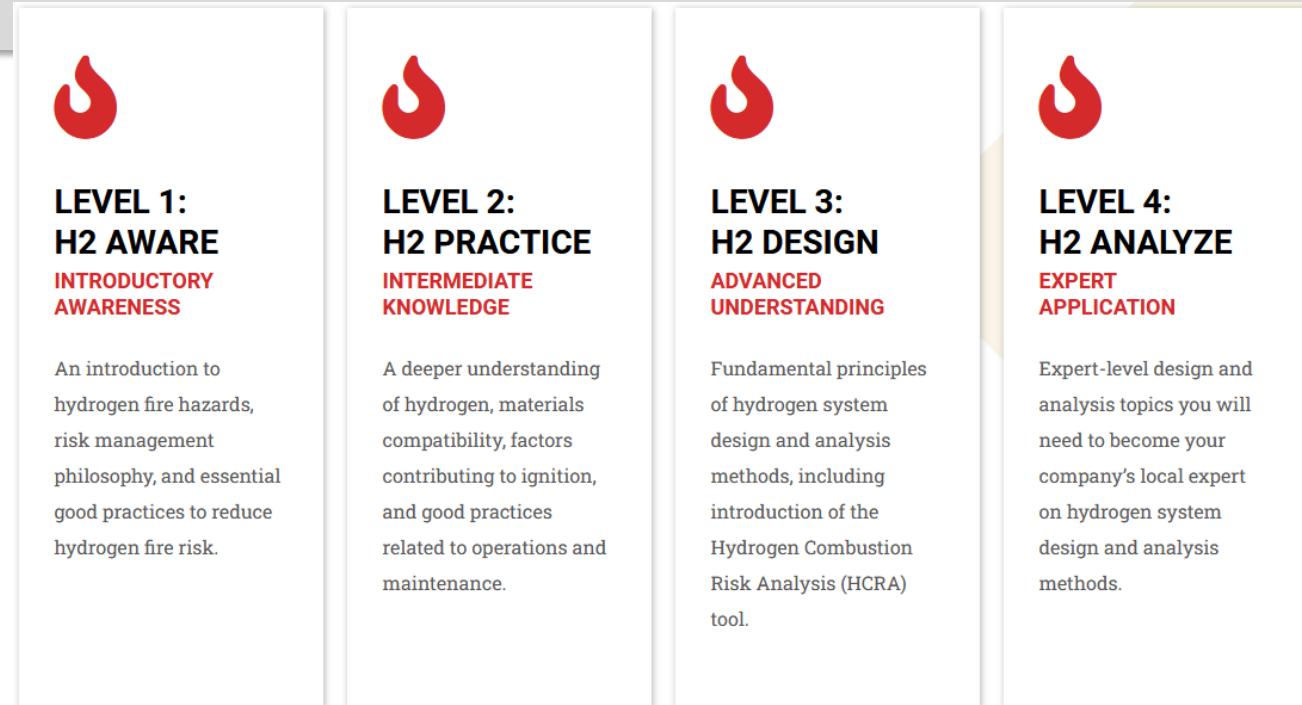
- ▶ [ELA201 Hydrogen as an Energy Carrier](#)
- ▶ [ELA202 Properties and Hazards of Hydrogen](#)
- ▶ [ELA203 Safety Planning for Hydrogen Projects](#)
- ▶ [ELA204 Safety Considerations for Hydrogen Facility Design and Construction](#)
- ▶ [ELA205 Safety Considerations for Hydrogen System Components](#)
- ▶ [ELA206 Safety Considerations for Liquid Hydrogen Systems](#)
- ▶ [ELA207 Material Compatibility Design Considerations for Hydrogen Systems](#)
- ▶ [ELA208 Hydrogen System Operation](#)
- ▶ [ELA209 Hydrogen System Maintenance and Inspection](#)





# Training and Hazard Analysis

Training with WHA International: <https://wha-international.com/training/>

In addition to training, we provide:

- ▶ Hydrogen systems design review
- ▶ Hydrogen component design review
- ▶ Risk analysis



 <p><b>LEVEL 1: H2 AWARE</b> INTRODUCTORY AWARENESS</p> <p>An introduction to hydrogen fire hazards, risk management philosophy, and essential good practices to reduce hydrogen fire risk.</p>	 <p><b>LEVEL 2: H2 PRACTICE</b> INTERMEDIATE KNOWLEDGE</p> <p>A deeper understanding of hydrogen, materials compatibility, factors contributing to ignition, and good practices related to operations and maintenance.</p>	 <p><b>LEVEL 3: H2 DESIGN</b> ADVANCED UNDERSTANDING</p> <p>Fundamental principles of hydrogen system design and analysis methods, including introduction of the Hydrogen Combustion Risk Analysis (HCRA) tool.</p>	 <p><b>LEVEL 4: H2 ANALYZE</b> EXPERT APPLICATION</p> <p>Expert-level design and analysis topics you will need to become your company's local expert on hydrogen system design and analysis methods.</p>
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**Hydrogen Combustion Risk Analysis:**

<https://wha-international.com/hazard-analysis/hydrogen-combustion-risk-analysis-hcra>

# Agenda – LH2 System Design

- ▶ System
- ▶ Deliveries
- ▶ Design Scope
- ▶ Locating Systems
- ▶ Equipment
- ▶ Codes and Standard



# System

- ▶ Delivered by LH2 delivery trailer into Cryogenic LH2 Tanks
- ▶ Cryogenic Liquid Tank
- ▶ Pumped and then vaporized **OR**
- ▶ Vaporized & compressed
- ▶ Stored onsite in intermediate storage
- ▶ Dispensed to the vehicle for fueling
- ▶ Safety Controls (LH2 only)



Liquid Hydrogen Delivery  
by Tanker Truck

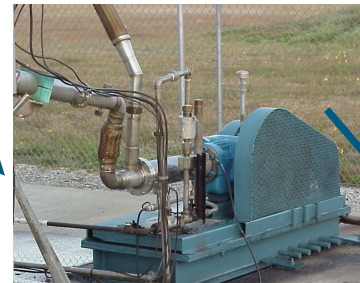


Liquid Hydrogen  
Storage Tank

OR



vaporizer



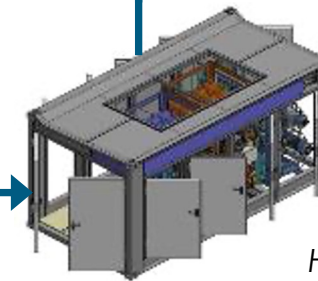
LH2 Pump

EITHER

Intermediate  
Storage



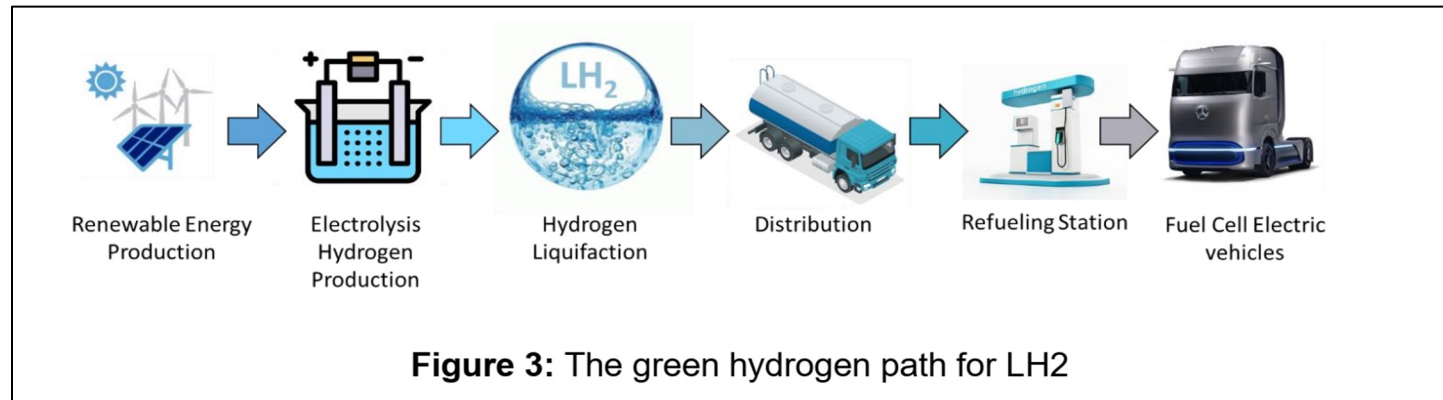
Hydrogen  
Dispenser



Hydrogen  
Compressor

# Deliveries

- ▶ Liquid Trailers
  - Medium to high usage – up to 25,000 kg/mo
  - Max pressure – 12 barg
- ▶ Pressure fill
- ▶ Pumped





# Design Scope

- ▶ Pressure - less than 8 bar to pumps
- ▶ Monthly throughput - Tank size/vaporizers
- ▶ Flow rate – Size pipe sizes
- ▶ Temperature range -253 C (-423 F) to ambient temperature
- ▶ # fills and how fast - provides operating time and flow rate
  - Sizes pumps/cycles, vaporizer, piping and storage tubes
- ▶ Determine Vent Losses – Cryogenics are typically “Use it or lose it”
  - Influence losses - Tank size, Pump cycles,
  - Recycle Compressor- reduces vent loss but a capital vs loss decision.



# Locating Systems

- ▶ Safe Locations incorporate
  - Safety setback distances (possibly with fire barrier walls) to minimize
  - Understanding the surroundings  
Protection from damage from vehicular impact from delivery tankers or other vehicles.
- ▶ Setback distances are based on fire exposure not for deflagration or detonation
- ▶ Vehicle access



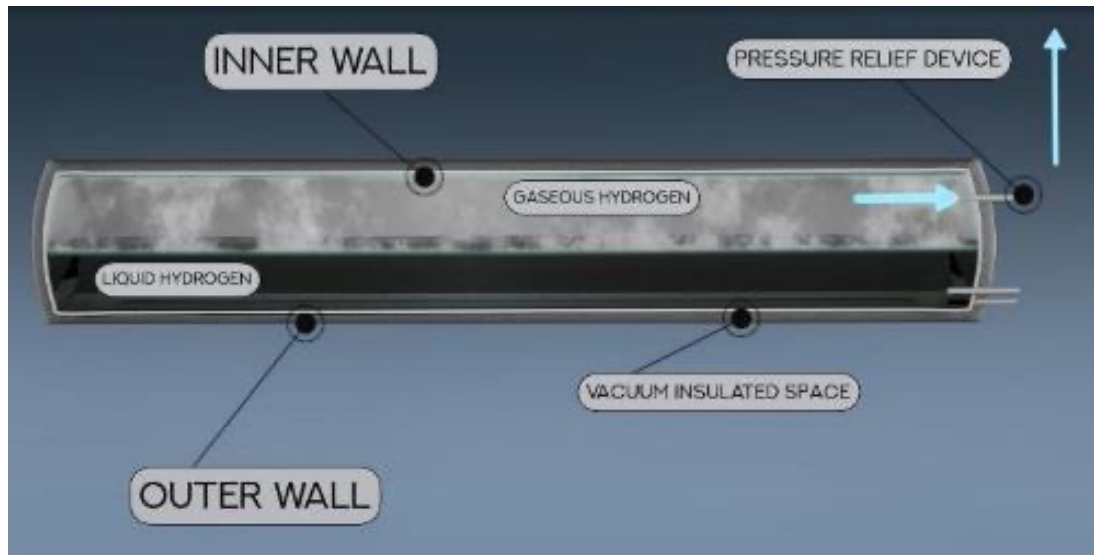
# Equipment

- ▶ Tank
- ▶ Vent Stack
- ▶ Vaporizers
- ▶ Pumps/Compressors
- ▶ Components
- ▶ Controls



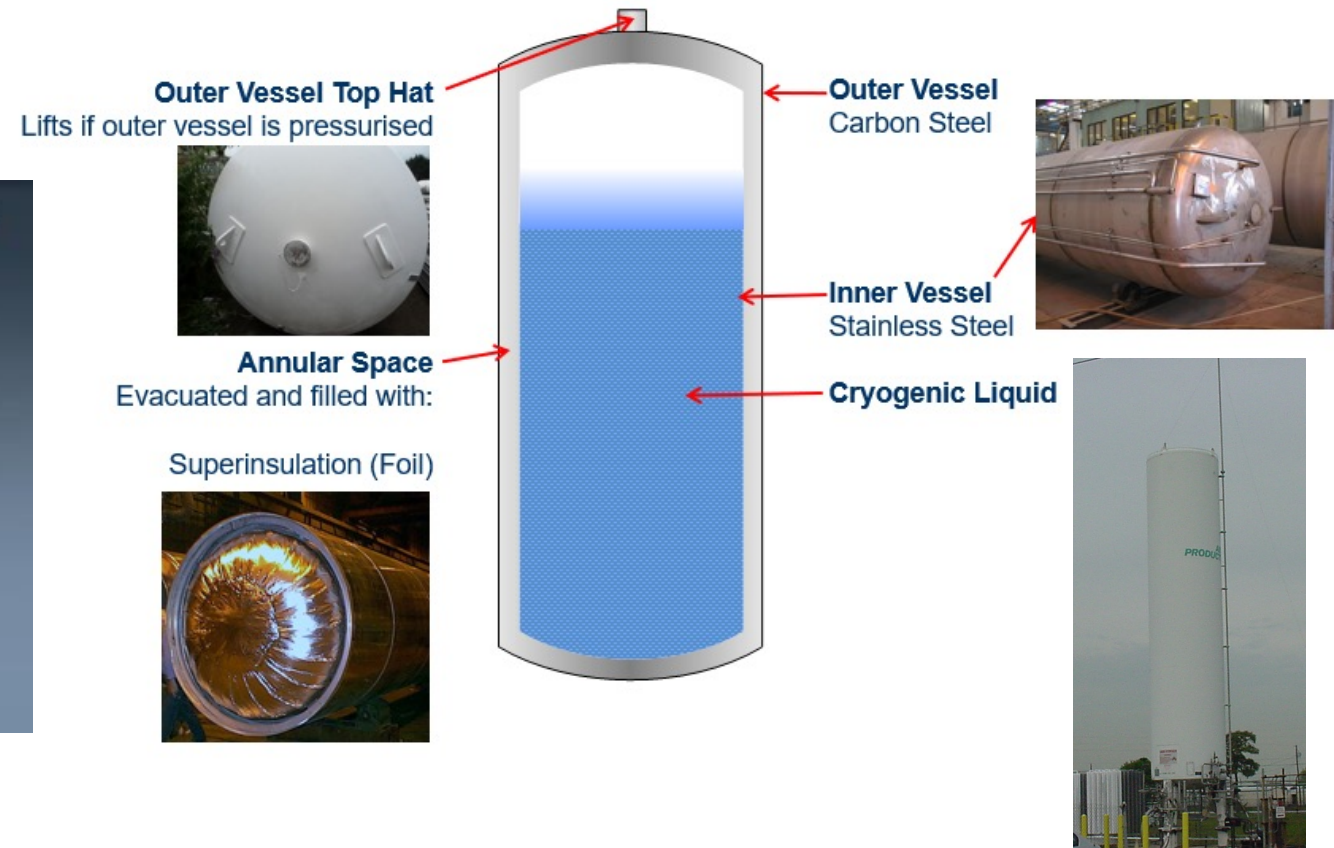
- ▶ Double walled vessels
- ▶ Vacuum Insulated

## Double walled vessels Vacuum Insulated



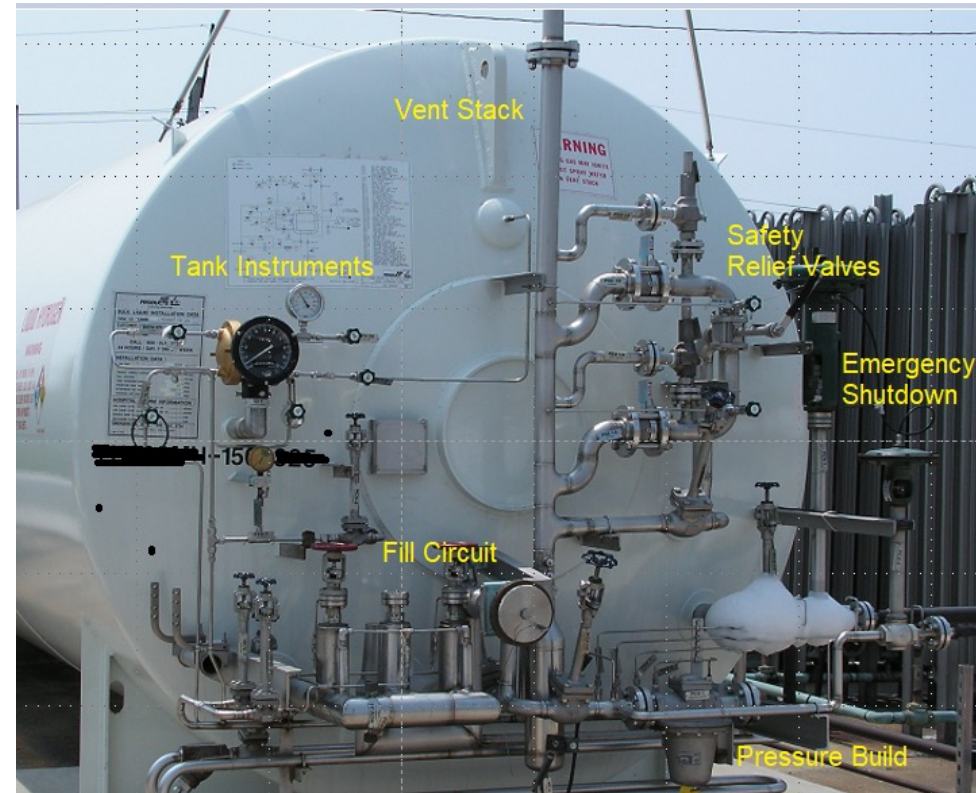
## Typical Cryogenic Tank Construction

- Cryogenic tanks are double walled and vacuum insulated

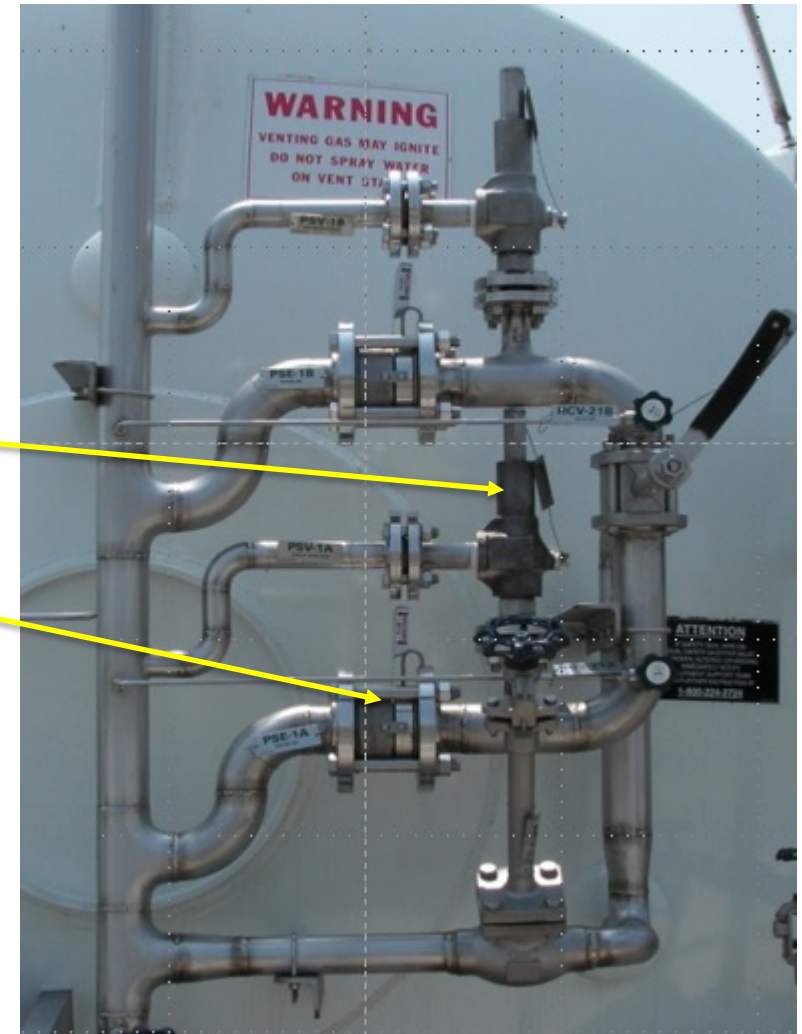
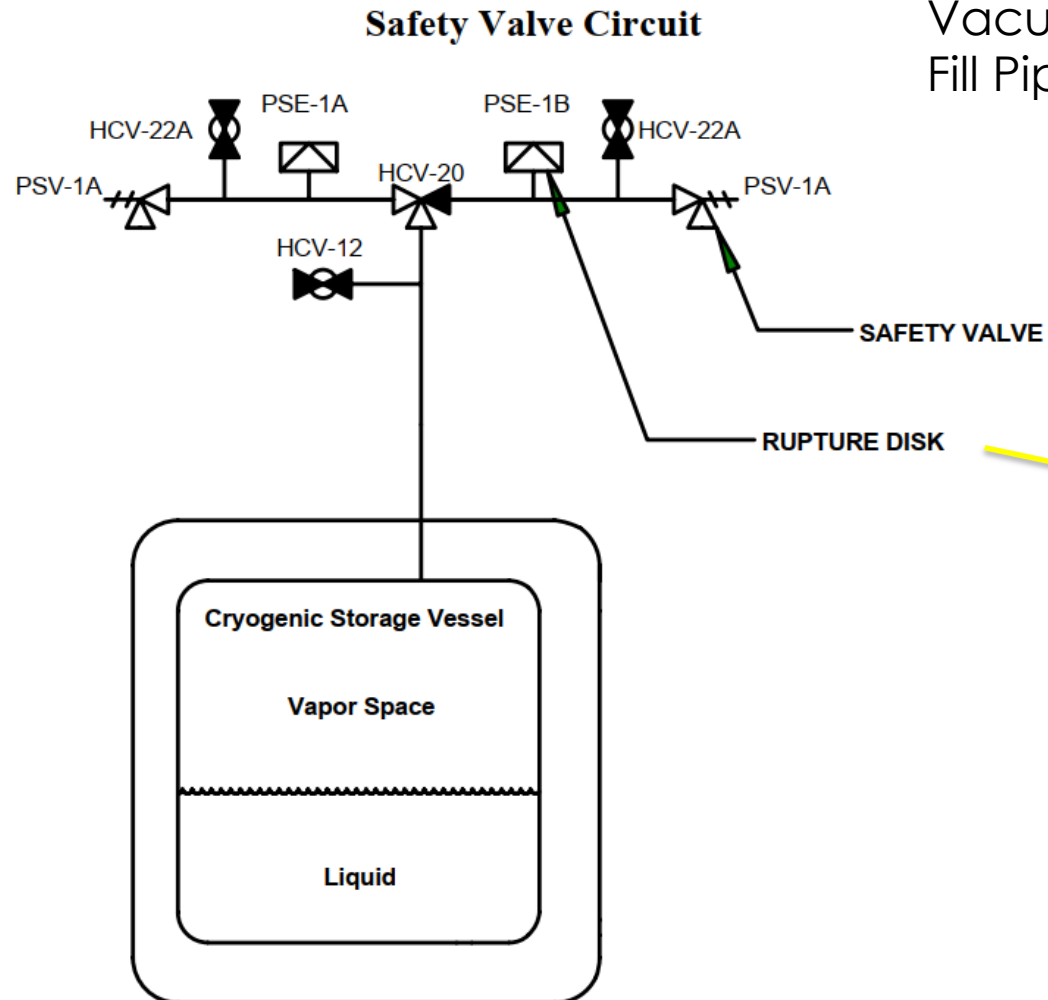


# Tank Circuits

- ▶ Safety Relief
- ▶ Fill Circuit
- ▶ Pressure Build
- ▶ Instrumentation
- ▶ Tank Vacuum
- ▶ Safety Control (i.e. Emergency Shutdown)



# Safety Relief Circuit

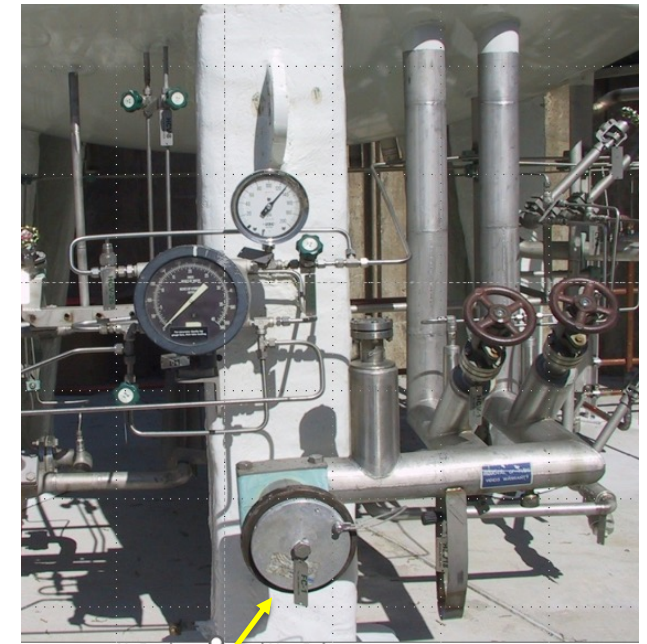
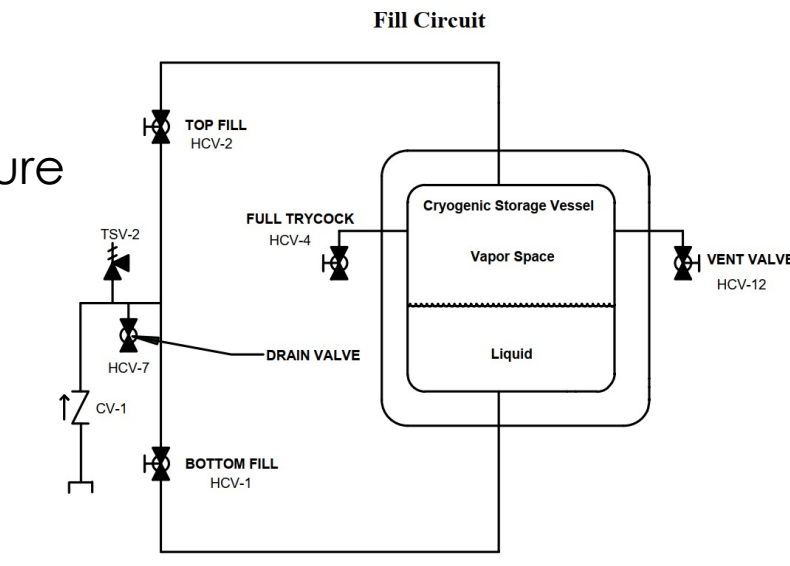


# Fill Circuit

- ▶ Tank is filled to Level and with Trycock valve
  - Key item, it's a safety issue to overfill
- ▶ Top and Bottom Fill
  - Top Fill - to reduce pressure
  - Bottom Fill - to increase pressure



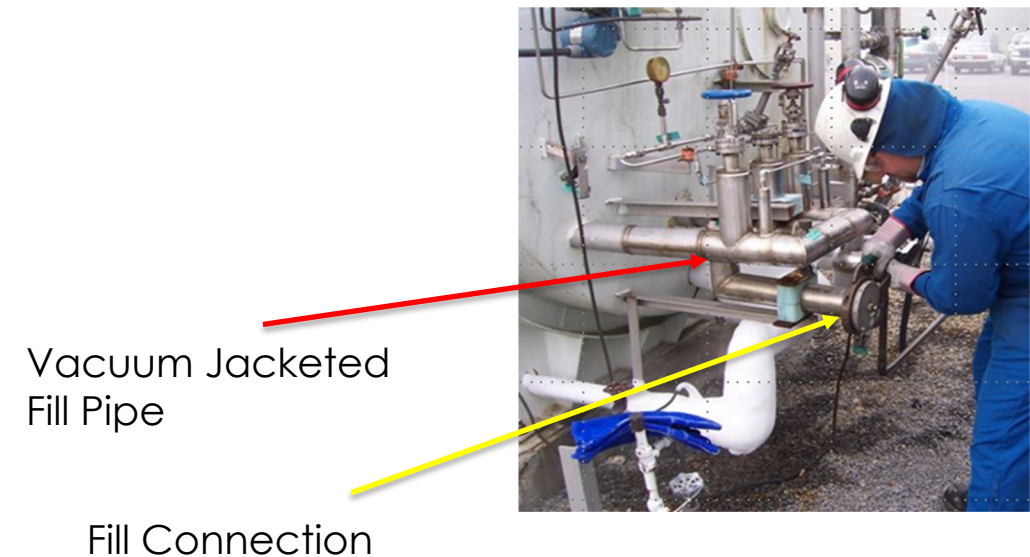
Vacuum Jacketed Fill Pipe



Fill Connection

# Fill Piping

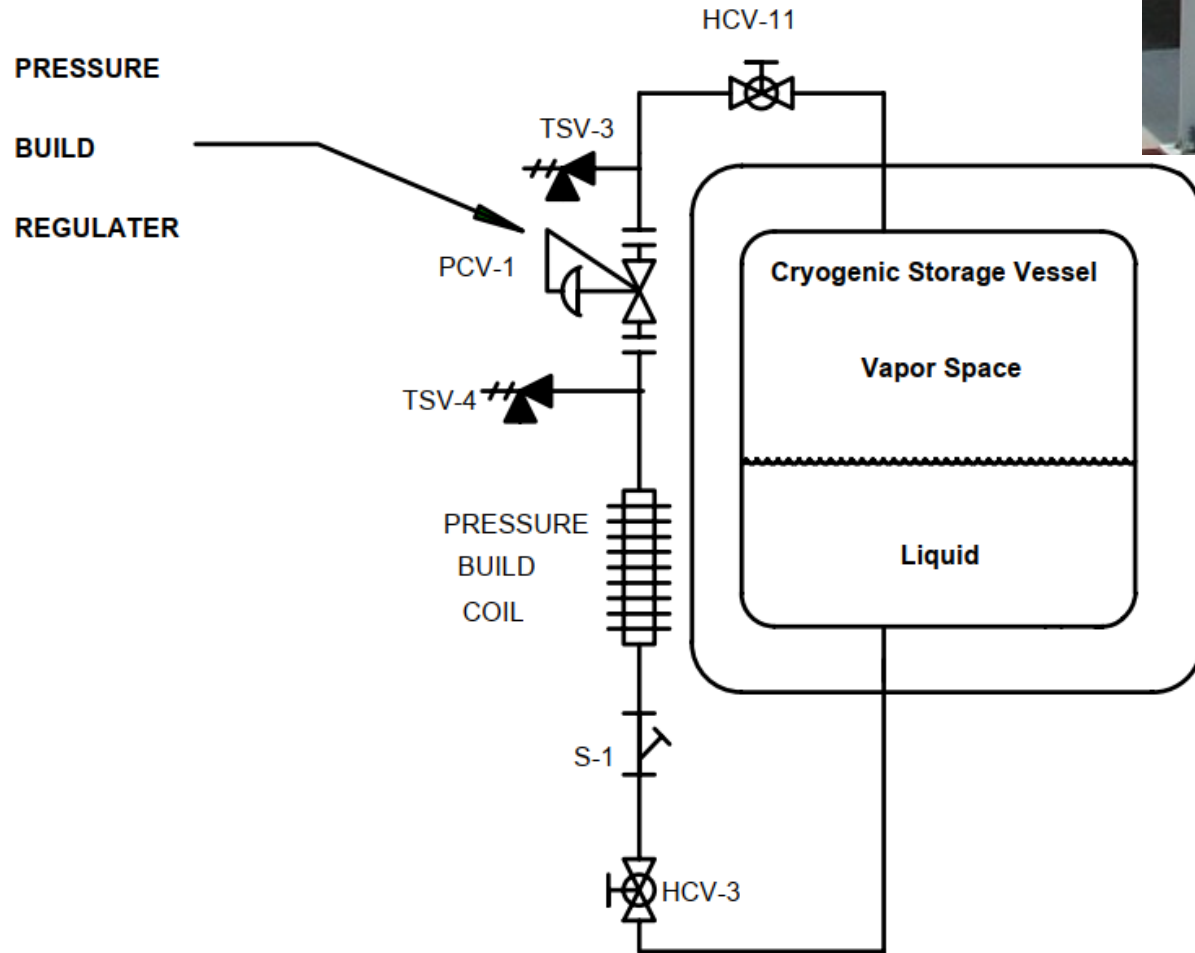
- ▶ Vacuum Jacketed Hose & Fill piping (Double wall)
- ▶ Fill Connection - Not standard
  - Bayonet, Vacuum Jacketed
    - Built for cryogenic temperatures
    - Reduce heat input and liquid air formation
    - NOT standardized
- ▶ Transfer Activity is manned by driver
  - Monitors Pressure and Liquid Level
  - Warm Hydrogen/Helium purging is needed at the beginning and end
  - Measuring Delivered Product - Flow meter or weight (scale nearby)





# Pressure Build

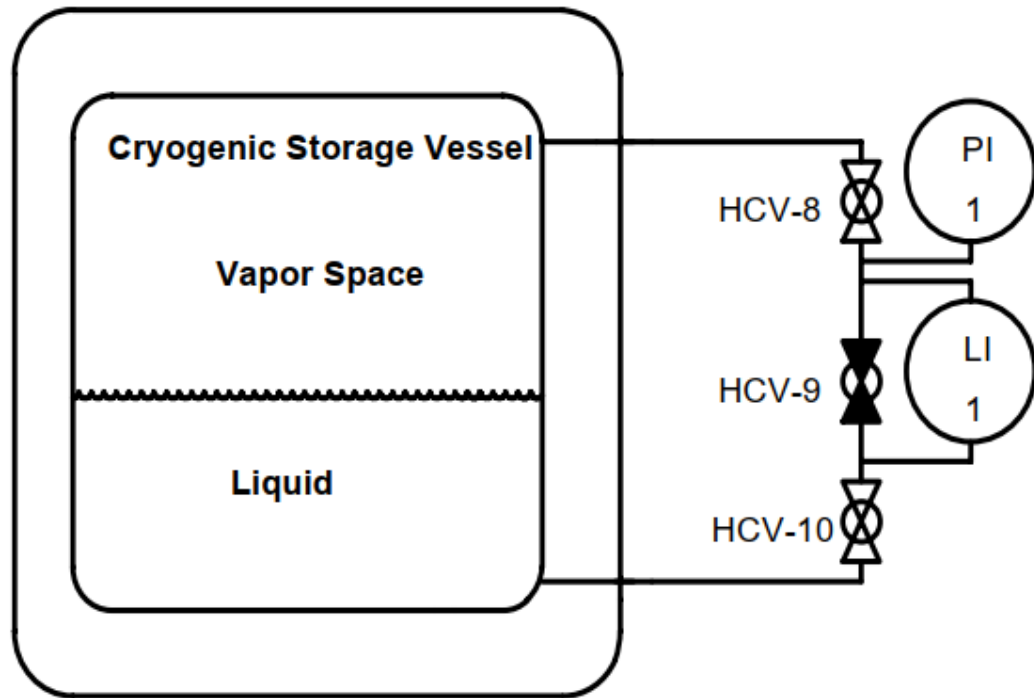
### Pressure Build Circuit



Pressure Build Heat Exchanger

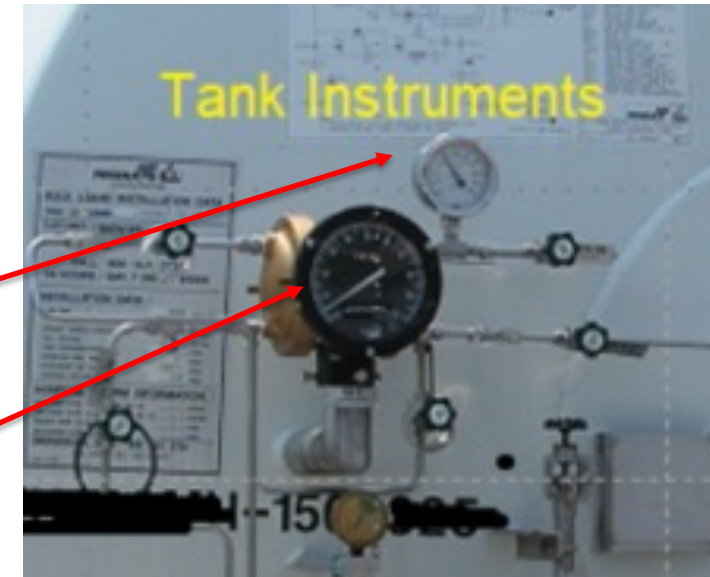
Pressure Build Regulator PCV-1

## Tank Instrumentation Circuit

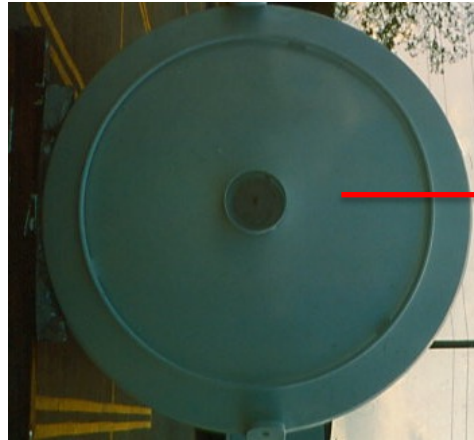


Pressure Gauge

Level Gauge



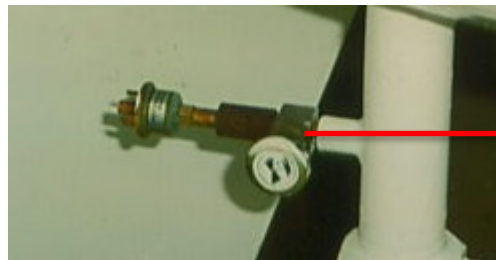
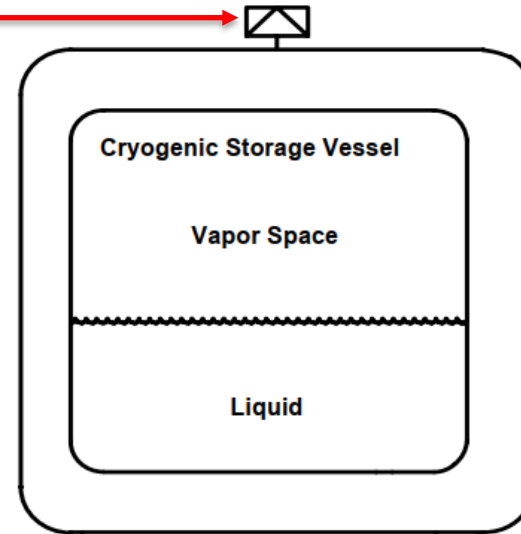
# Vacuum Circuit



Relief Device

## Tank Vacuum Circuit

OUTER VESSEL RELIEF DEVICE



Probe to Check Vacuum

HCV-5  
VACUUM  
PROBE  
VR-1

HCV-6

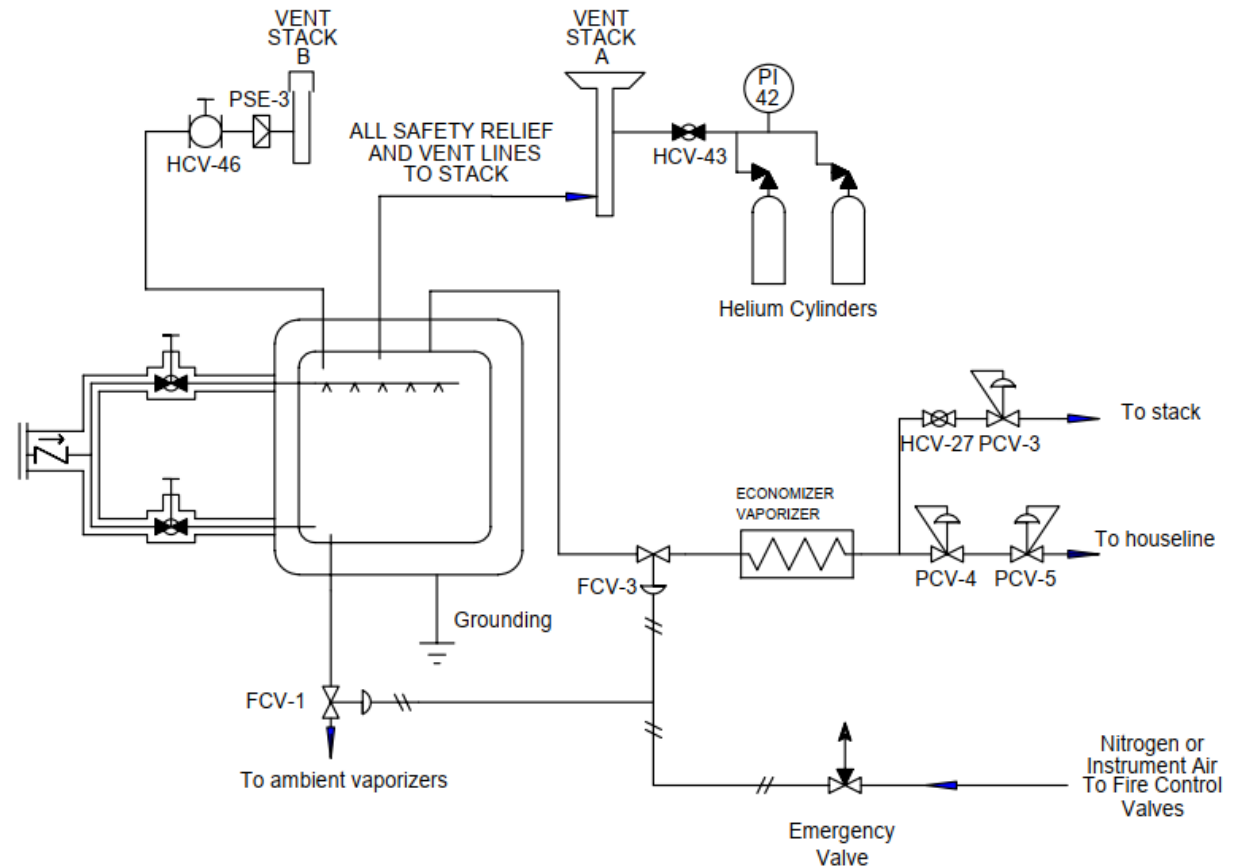
Vacuum Pump out



# Controls/ Emergency Shutdown

- ▶ Isolation valves (Estops)
- ▶ Vent component set to vent stack
- ▶ Secondary stack vent stack
- ▶ Equipment grounded and bonded
- ▶ Purge gas
- ▶ Electrical components designed for hydrogen (Atex or NFPA 70)

### Hydrogen Tank Features



# Liquid Hydrogen Venting

- ▶ More complex than GH2
- ▶ Elevated higher than GH2 to 25 ft
- ▶ Allows H2 to warm and disperse
- ▶ Cryopump air when cold inside (Moisture inside pipe)
- ▶ Liquid air condensation



# Vaporizers

- ▶ Convert LH2 to gas
- ▶ Warm to near ambient temperatures
- ▶ Can be overdrawn with too much flow in continuous service and/or cold wet weather
- ▶ Safety - Low temperature, fog, and ice issues



# Vaporizer Safety Issue

- ▶ Falling Ice
- ▶ Fog
- ▶ Low Temperature



# Vaporizer – Low Temperature





# Compressors/ Pump

- ▶ Compressors - Gaseous hydrogen (GH<sub>2</sub>) pressure increase
- ▶ Compressors can be driven by electric motors or pneumatically
  
- ▶ LH<sub>2</sub> Pump
  - LH<sub>2</sub> pressure increase
  - Pumps are driven by electric motors. Electric motors have to meet electrical classification

Compressor



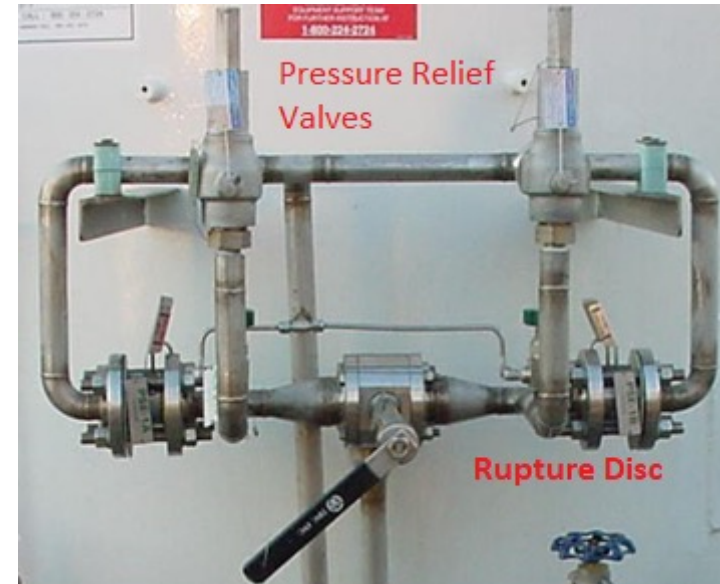
Pneumatic Gaseous Hydrogen Compressor



Cryo pumps

# Component Design

- ▶ Relief Devices
- ▶ Expansion/ contraction design



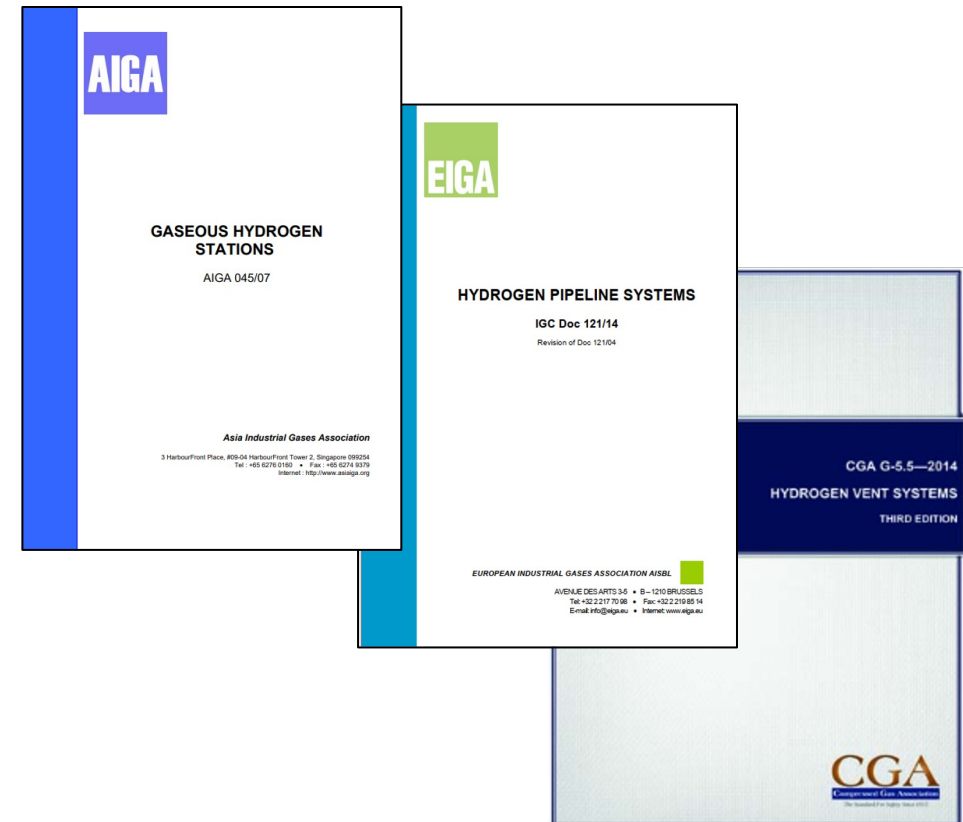
# Safety Controls

- ▶ Emergency Shutoff
- ▶ Low-Temperature Shutdown
- ▶ Pressure Relief Devices where liquid can expand and overpressure the system
- ▶ Pumps – High pressure and high temperature ~ -160 C (-256 F) shutdowns
- ▶ Compressors – high pressure and high temperature ~ 150 C (300 F)
- ▶ Electrical Classification – means to control ignition sources in flammable/explosive environments
  - Atex – Zone 1 or 2 (ATEX Directive for controlling explosive atmosphere (Europe))
  - NEC – Class 1, Division 1 or 2, Group B (National Electric Code (aka NFPA 70) (North America))
- ▶ Grounding and Bonding



# Codes and Standards

- ▶ Asian Industrial Gas Association (AIGA)
  - ▶ Compressed Gas Association (CGA)
    - H-5 – Standard for Bulk Hydrogen Supply Systems
    - H-3 Standard for Cryogenic Hydrogen Storage
    - G5.4 - Standard for Hydrogen Piping Systems at User Location
    - G5.5 – Hydrogen Vent Systems
  - ▶ European Industrial Gas Association (EIGA)
    - Doc. 211/17 Hydrogen Vent Systems for Customer Applications
  - ▶ National Fire Protection Association (NFPA)
    - NFPA 2 - Hydrogen Technologies Code
    - NFPA 70 (NEC) – Article 500



# Codes, Standards & Regulation

## ▶ Global

- ISO – International Standards Org
  - [ISO 13984](#) Liquid hydrogen – Land vehicle fueling system interface
  - [ISO 13985](#) Liquid hydrogen - Land vehicle fuel tanks
  - [ISO/TR 15916](#) Basic consideration for the Safety Hydrogen Systems
- Global Technical Regulations GTR 13 - Hydrogen and Fuel Cell Vehicles
- United Nations
  - Work Party 29 Global Regulations on Pollution and the Environment Global Technical Regulations (GTR) - Hydrogen

[Hydrogen Fuel Cell Codes & Standards \(fuelcellstandards.com\)](https://fuelcellstandards.com)

# Thanks for Your Attention!



[www.WHA-international.com](http://www.WHA-international.com)

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*CHS... Bringing together individuals and organizations to develop and share best safety practices and learnings*

# Questions?

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<http://www.aiche.org/chs>

<http://h2tools.org>

