#### **ECCE 10**

### INFLUENCE OF INITIAL TURBULENCE AND CONCENTRATION ON DUST EXPLOSIONS:

A Combination of Computational and Experimental Approaches

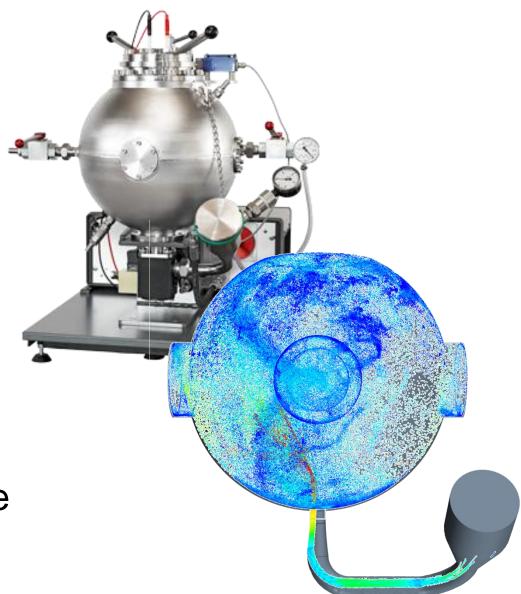
**Presented by:** 

<u>Carlos Murillo</u>, Nathalie Bardin-Monnier, Felipe Muñoz, Daniel Vizcaya, Christian Blanchard & Olivier Dufaud

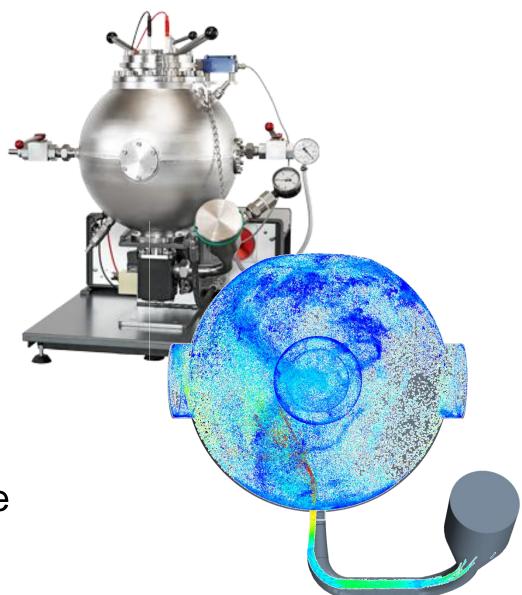




- Introduction
- Experimental description of dust dispersion
- Computational description of dust dispersion
- Conclusions & Future Work



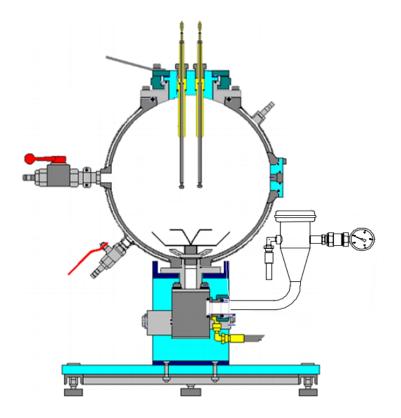
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### Flammability tests in the 20-L sphere

Determination of flammability parameters of combustible dusts:

- Minimum Explosible Concentration (MEC)
- Maximum pressure rise (P<sub>max</sub>)
- Maximum rate of pressure rise (dP/dt)<sub>max</sub>



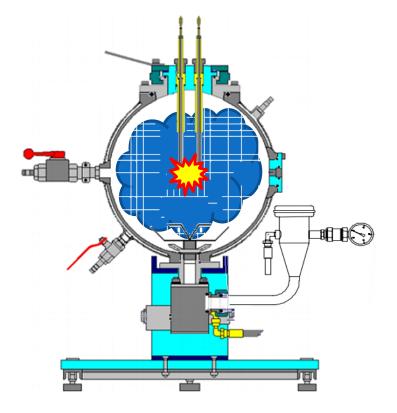
**20-L Apparatus** ASTM E2019-03 IEC 241-2-3, 1994

### Flammability tests in the 20-L sphere

- Fairly uniform dust cloud of the material
- **Injection** of the dust-air mixture in a spherical vessel.
- Ignition of the dust cloud (60 ms)

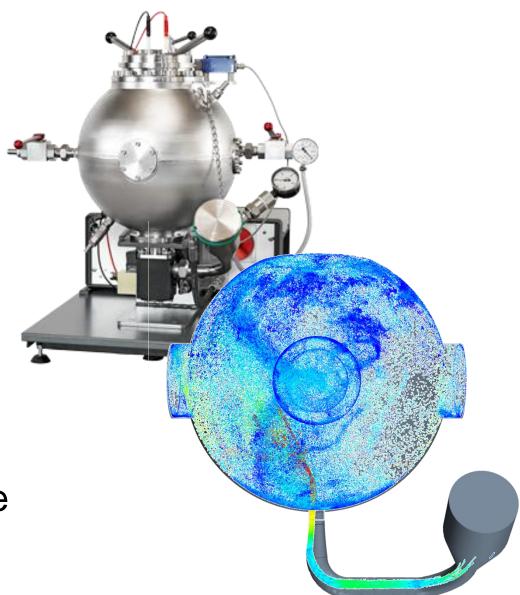
#### CHARACTERIZATION OF DUST DISPERSION

- Aerodynamics of the two-phase flow
- Uncertainty levels of the test
- Propagation of the combustion flame



**20-L Apparatus** ASTM E2019-03 IEC 241-2-3, 1994

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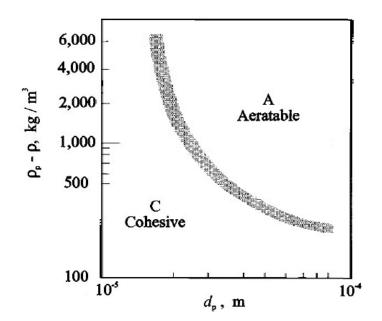
### Fluidization of wheat starch

Particle's diameter (µm)	Archimedes Number (Ar)
29	3.3
37	7.5
65	41.2
81	78.1
83	85.2
87	96.6

$$Ar = \frac{d_p^3 \rho_f \quad \rho_p - \rho_f \quad g}{\mu^2}$$

 $\rho_{ad} = \rho_p - \rho_f / \rho_f$ 

#### **MODIFIED GELDART'S CLASSIFICATION OF POWDERS**



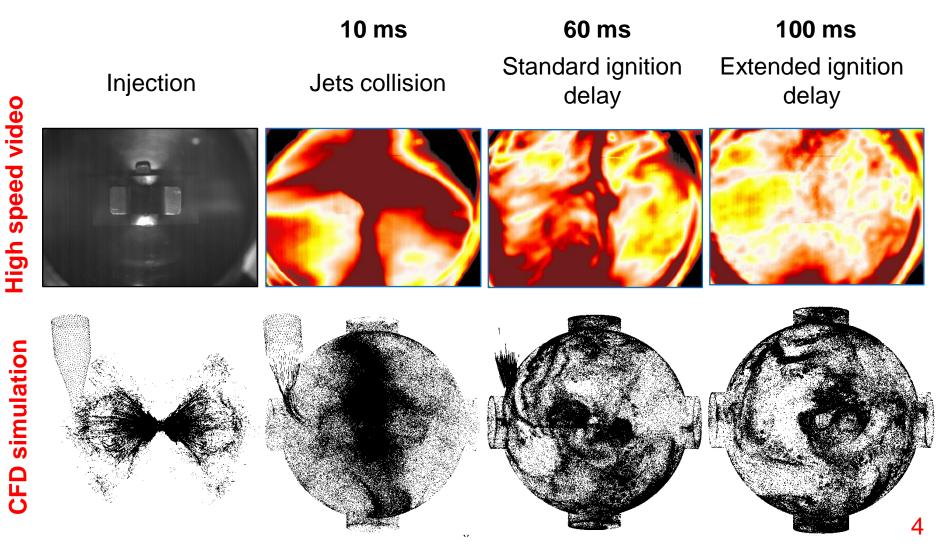
#### **Group A:**

Several desirable fluidization characteristics. They expand homogeneously in fluidized beds.

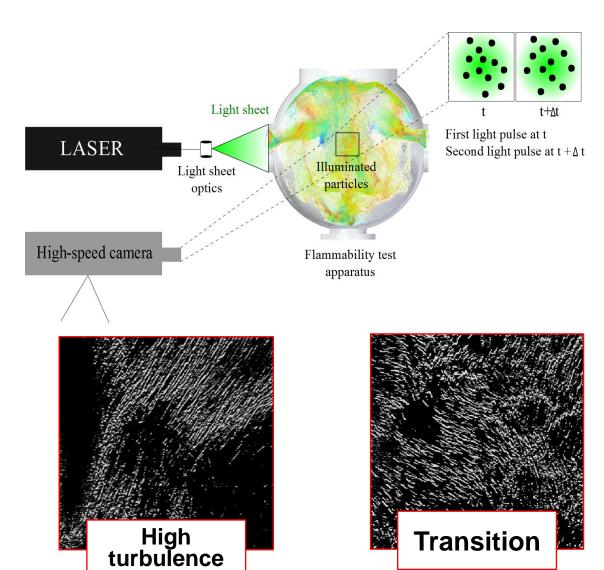
#### Group C:

Difficult fluidization characteristics. Cohesive behavior

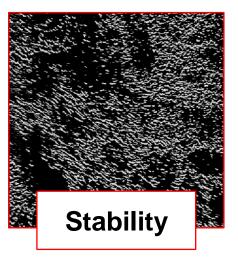
# Dispersion of micrometric wheat starch within the 20-liter sphere



### Particle Image Velocimetry

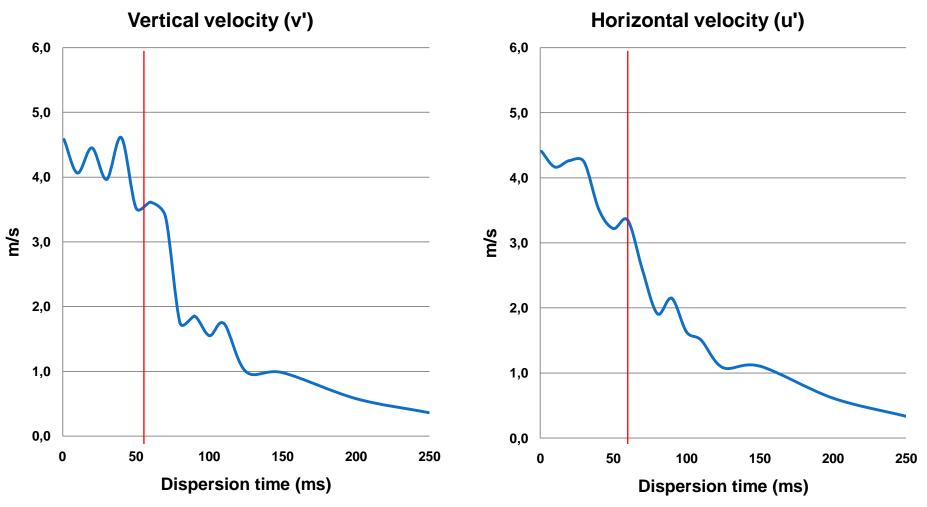


- The settings of the camera were adjusted to visualize a region of 3.0 cm x 3.0 cm.
- Framerate: 6,400 fps (0.16 ms).

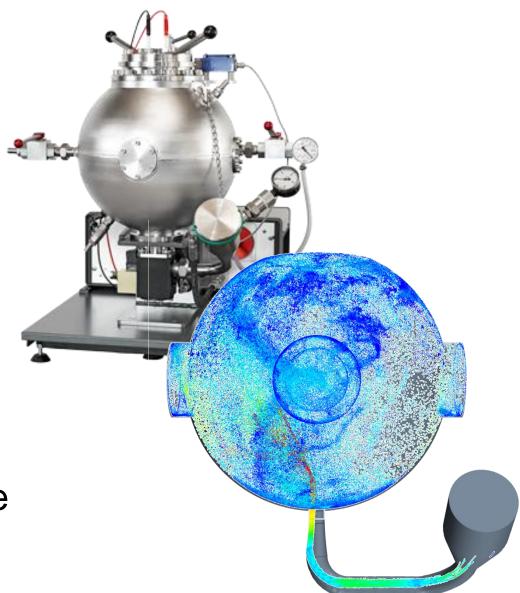


### Particle Image Velocimetry





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Computational Fluid Dynamics EULER-LAGRANGE APPROACH

#### $(\Phi_{\text{SOLIDS}} < 10\%)$

#### **CONTINUOUS PHASE** (EULERIAN) Dispersion gas

#### Navier-Stokes equations

*Turbulence model: Detached Eddy Simulations.* RANS model: Boundary layer LES model: Core region of the fluid flow



#### DISCRETE PHASE (LAGRANGIAN)

Combustible dust

#### Momentum balance

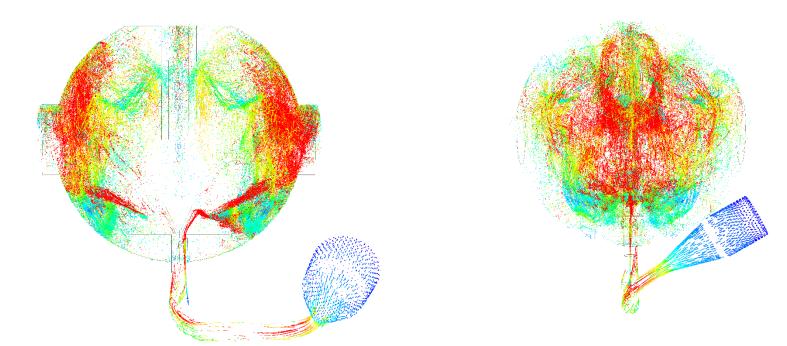
- -Drag force (Relative velocity)
- -Shear lift force
- -Pressure gradients

-Coefficients of restitution (particles & walls) Normal:0,25 Tangential:0,20

### **Computational results**

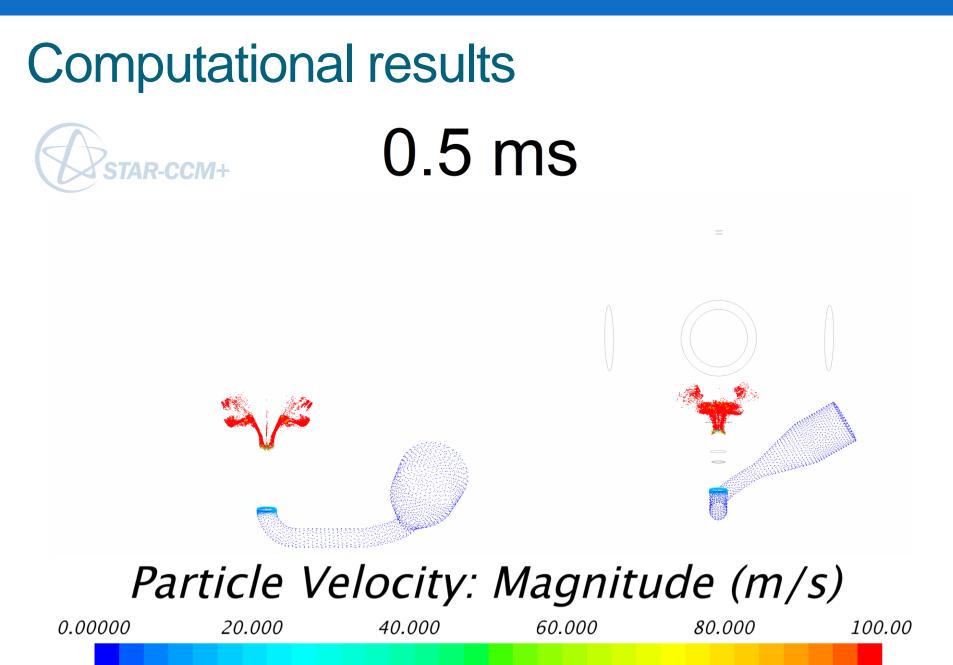


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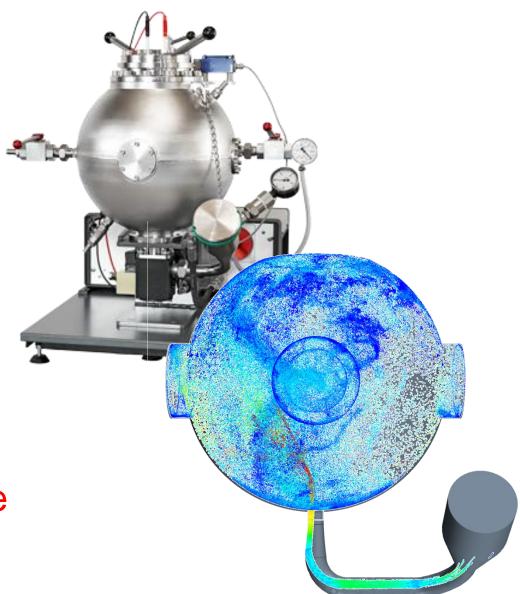


### Particle Velocity: Magnitude (m/s)

0.00000	20.000	40.000	60.000	80.000	100.00



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- The ignition delay for micrometric wheat starch must be established between 60 and 80 ms.
- The computational analyses can become a useful tool for the development of a flammability test due to their capability of describing the development of a combustible cloud.



### Perspective

- Compare different types of combustible dusts in order to characterize properly the influence of their physical properties
- Develop a comparative analysis of diverse injection nozzles to identify new alternatives that provide more uniformity and stability to the dust cloud



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