

#### Pilot Test Results from a Polaris<sup>TM</sup> Membrane 1 MW<sub>e</sub> CO<sub>2</sub> Capture System

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## **MTR Introduction**

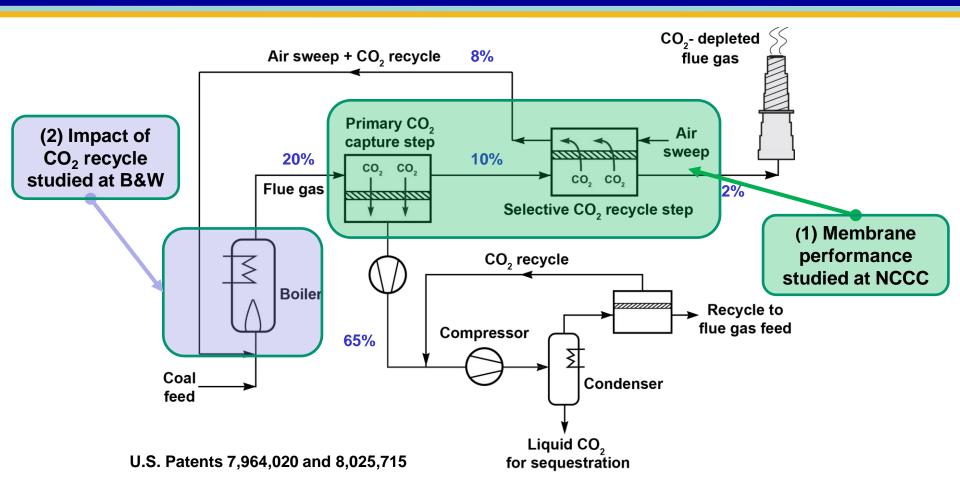


- Privately-held, 60 employees mostly located in Newark, California
- Started in 1982 funded by U.S. SBIR grants
- Commercial products in petrochemical, natural gas and refinery industries
- Provides complete turn-key solutions with over 200 membrane systems installed worldwide
- 15 person R&D group with expertise in membrane materials/formation and process design





# **Background: MTR CO<sub>2</sub> Capture Process**

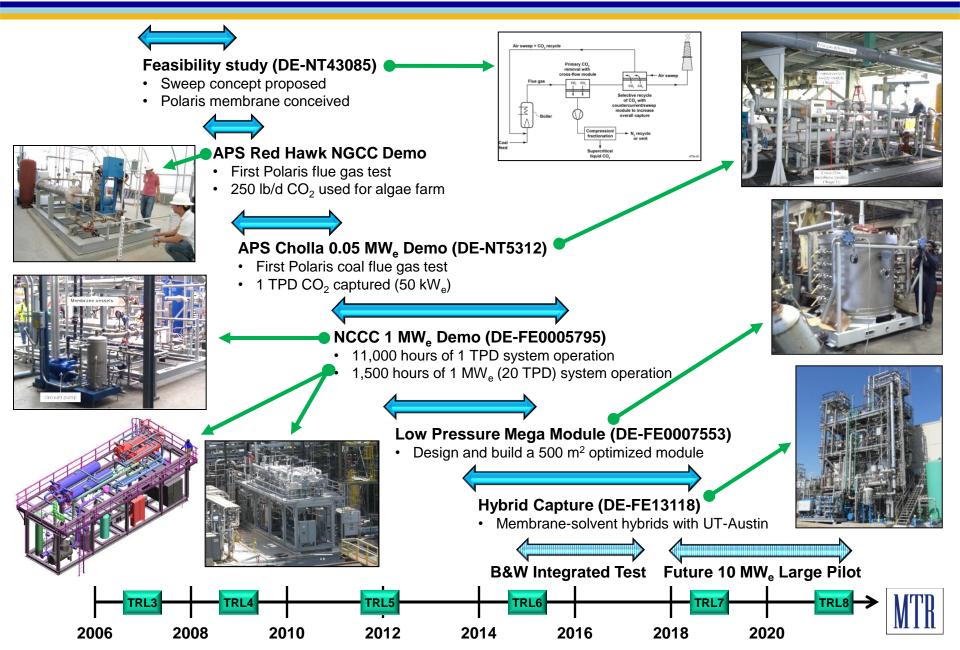


#### Benefits of selective recycle:

- Increases CO<sub>2</sub> concentration going to the capture step, and
- Reduces the fractional CO<sub>2</sub> removal required by the capture step



## **MTR CO<sub>2</sub> Capture Development Timeline**



## Pros and Cons of a Membrane Post-Combustion Capture Process

#### **Benefits:**

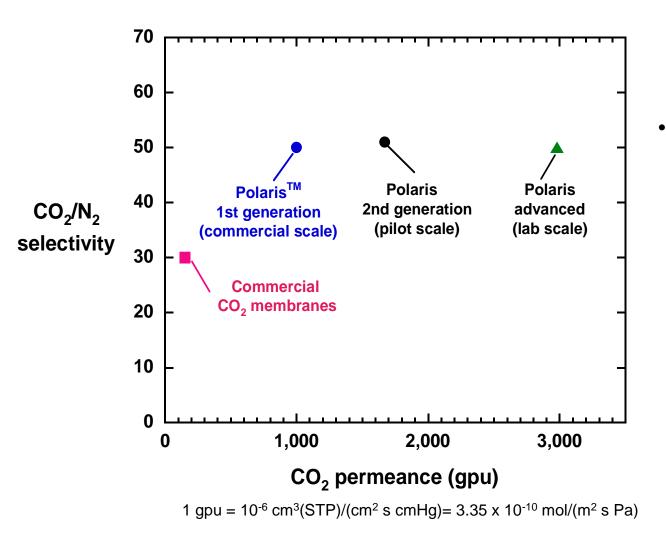
- No hazardous chemical handling, emissions, or disposal issues
- Not affected by oxygen, SO<sub>x</sub> or NO<sub>x</sub>
- Water use lower than other technologies (recovers H<sub>2</sub>O from flue gas)
- No steam use  $\rightarrow$  no modifications to existing boiler/turbines
- Near instantaneous response; high turndown possible
- Modular and compact; relatively simple installation/operation
- Particularly well-suited for partial capture (40-60%)

#### Challenges:

- Very low partial pressure driving force favors high permeance membranes
- Unknown impact of real flue gas on membrane-module lifetime
- Module pressure drop and flow distribution issues



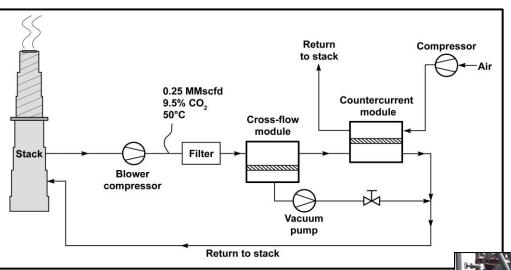
#### **Polaris<sup>™</sup> Membranes Continue to Improve**



In addition to lowering costs, these improvements are important to shrink the size of the capture system

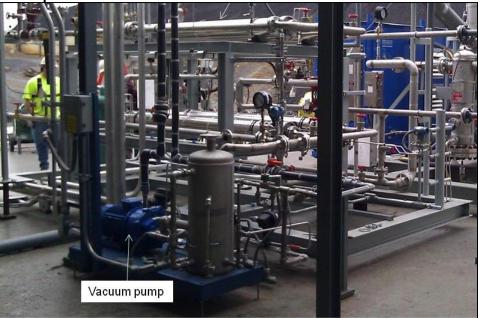


# 0.05 MW<sub>e</sub> (1 TPD) Testing at NCCC



- System is testing vacuum and air sweep membrane steps
- Sized to capture 1 ton CO<sub>2</sub>/day using commercial sized module
- System was in operation from Spring 2012 through Summer 2015

- Field laboratory that allows lifetime evaluation (>11,000 hours cumulative), and validation testing of new membranes
- Many lessons learned (i.e., ammonium sulfate deposition) applied to scale up



# 1 MW<sub>e</sub> (20 TPD) System at NCCC



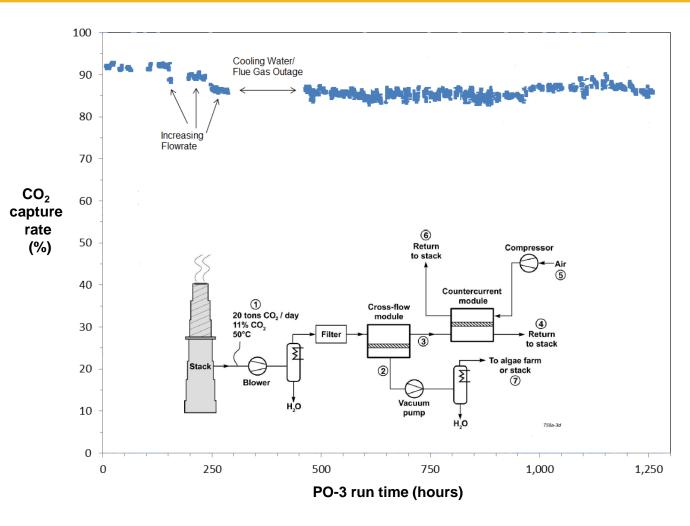
 System showed stable performance over 1,500 hours of operation, including demonstration of prototype low-pressure drop plateand-frame sweep modules

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- System installation completed Aug 2014
- Operation during January June 2015
- Decommissioned in July 2015



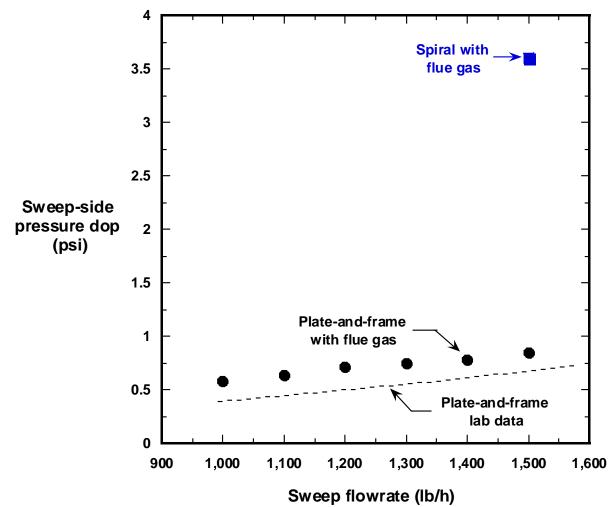
## 1 MW<sub>e</sub> System Shows Stable Performance



- System operated in slipstream mode (no recycle to boiler) with varying ambient conditions (sub-freezing in January to >95°F in June)
- Stable performance, reaching up to 90% capture
- System goes from cold start to steady state in ~15 minutes

#### Figure data from NCCC campaign PO3 (May to July 2015)

## New Modules Demonstrate Improved Pressure Drop Performance



- Field data is consistent with lab results, and confirms much lower air sweep pressure drop in new modules
- At full scale, the difference in pressure drop amounts to savings of about 10 MW<sub>e</sub>



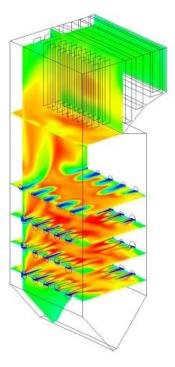
#### **B&W Studies of CO<sub>2</sub> Recycle Impact** on Boiler Performance

#### Phase I – CFD modeling

- B&W modeled 2 boiler configurations (radiant boiler firing bituminous coal and SWUP firing PRB coal) and 2 sweep recycle cases (constant secondary air flow and constant stoichiometry)
- <u>Main conclusion of modeling study</u>: secondary air laden with CO<sub>2</sub> appears feasible as a retrofit in either of the boiler configurations examined if oxygen mass flow to boiler is fixed

#### Phase II – Pilot testing

- B&W's SBS-II 1.8 MW<sub>th</sub> pilot boiler operated with CO<sub>2</sub>-laden combustion air
- Two coals evaluated: a western sub-bituminous coal and a highly volatile bituminous coal
- $O_2$  content of windbox air varied from 21% to 16% through  $CO_2$  dilution
- Monitored flame stability, length, and shape; unburned combustibles in fly ash, and furnace exit gas temperature
- Radiant furnace and convective pass heat absorptions were measured
- Boiler efficiencies for air and sweep firing were determined





# **B&W Boiler Study Highlights**

- Stable and attached flames with air (21% O<sub>2</sub>) and CO<sub>2</sub>-enriched air (16-18% O<sub>2</sub>)
- CO<sub>2</sub>-enriched flame was less luminous than air-fired case
- Lower furnace heat absorption but higher convection pass/air heater heat transfer for CO<sub>2</sub>-enriched operation relative to air
- For bituminous coal, 30% lower NO<sub>x</sub> emissions with CO<sub>2</sub>-enriched air
- No burner modifications necessary
- Net reduction in plant efficiency of ~0.75% at 18% O<sub>2</sub>

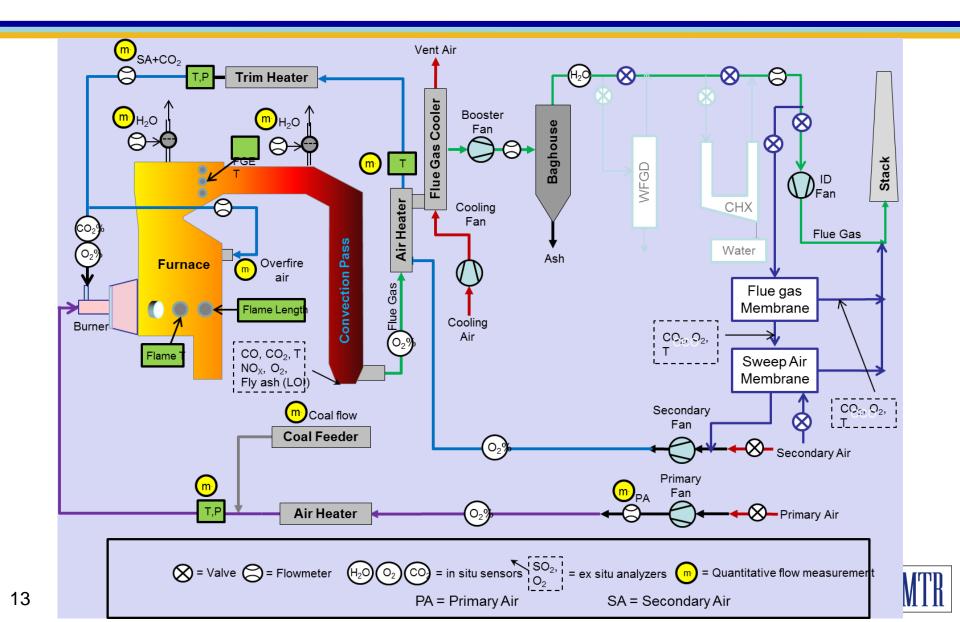
Flame image from combustion of PRB coal with air (21% O<sub>2</sub>)



Flame image from combustion of PRB coal with  $CO_2$ -enriched (18%  $O_2$ )



## **B&W Pilot Boiler / Membrane Schematic**



## MTR Skid During Transport and Installation at B&W – May 2016

#### Skid arriving at B&W ——



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#### —— Installation of 2<sup>nd</sup> floor



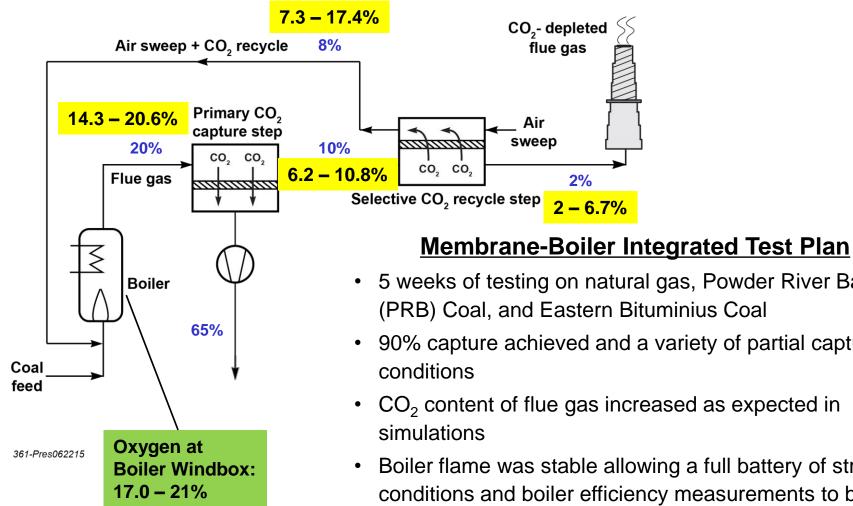
#### MTR Skids at B&W's SBS-II Research Facility



Main skid and smaller low-pressure drop sweep module anchored to foundation



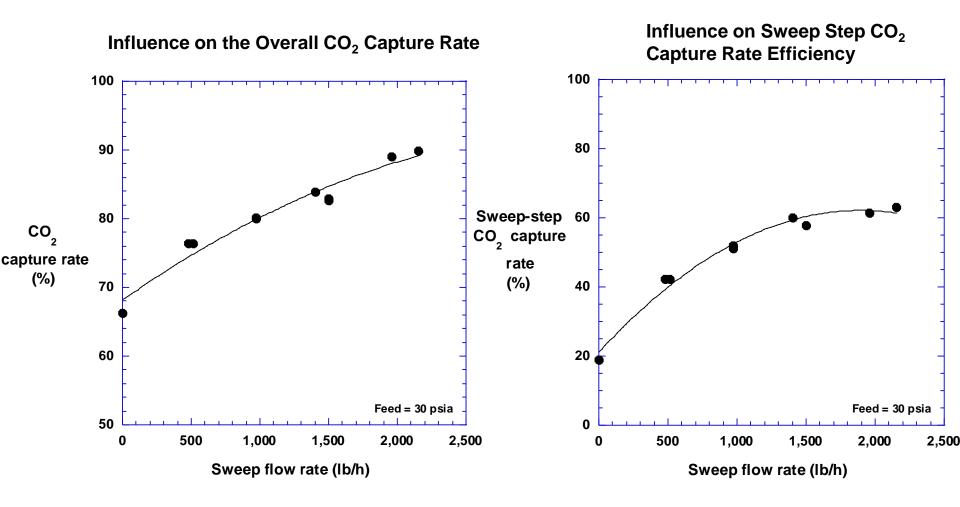
## Sample Results from B&W **Integrated Tests**



5 weeks of testing on natural gas, Powder River Basin

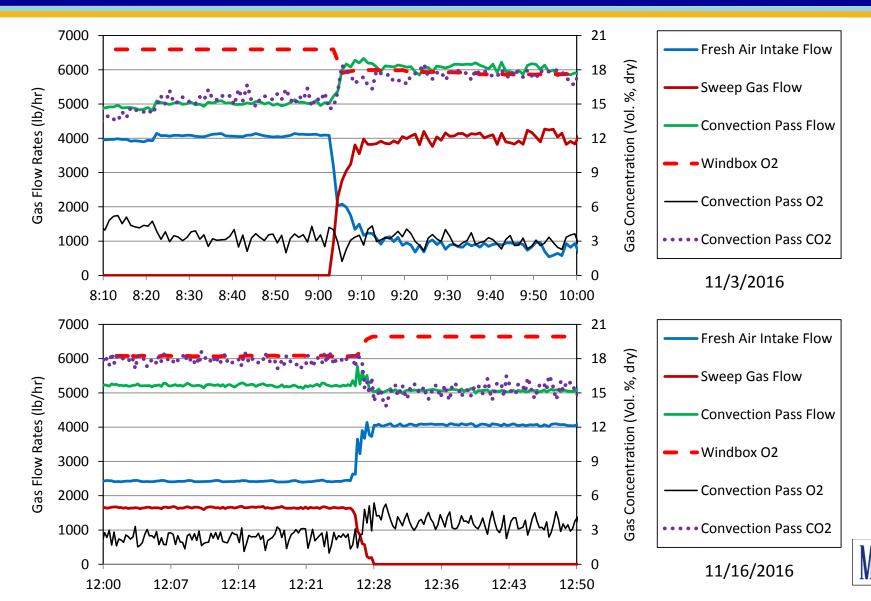
- 90% capture achieved and a variety of partial capture
- CO<sub>2</sub> content of flue gas increased as expected in
- Boiler flame was stable allowing a full battery of stream conditions and boiler efficiency measurements to be conducted (analysis is ongoing)

#### 1 MW<sub>e</sub> System Sweep Flow Rate Parametric Results from Integrated Tests

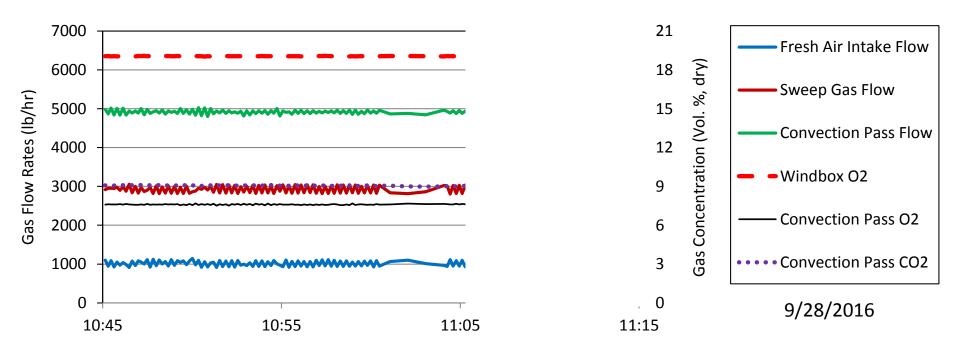




## Integrated Boiler/Membrane Systems Transition Response



## Integrated Boiler/Membrane Systems Transition Response to E-Stop

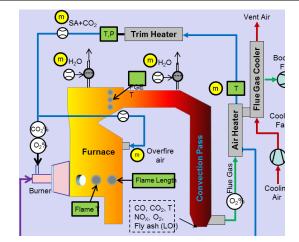




## **B&W's Analysis of CO<sub>2</sub> Recycle Impact on Boiler Operation**

- Furnace heat absorption is lower resulting
- "Furnace" refers to the radiant heat transfer section of the boiler upstream of the tube banks in the convection pass.
- Convection pass heat
  absorption is higher
- Convection pass outlet heat flux is higher
- Air heater heat absorption is higher
- Air heater flue gas outlet heat flux is higher
- Total heat absorption is slightly reduced

Test Name		Coal 30P M1 & M2	Coal 27P M2 Only
Date		20-Oct-16	18-Oct-16
Test Duration	(h:mm)	7:00	7:15
Fuel		PRB	PRB
Load	(MW)	1.5	1.4
FEGT	(°C)	1,179	1,259
Convection Pass Exit Temperature	(°C)	397	380
Air Heater Exit Temperature (Flue Gas)	(°C)	217	210
Membrane Secondary Air Ratio		53%	0%
Furnace Absorption	(MW)	0.52	0.66
Convection Pass Absorption	(MW)	0.96	0.91
Convection Pass Outlet Heat Flux	(MW)	0.50	0.43
Total Heat Absorption	(MW)	1.62	1.68
Air Heater Absorption	(MW)	0.19	0.16
Air Heater Outlet Heat Flux (Flue Gas)	(MW)	0.31	0.27





## Summary

- CO<sub>2</sub> capture membrane performance continues to improve and has been validated on the 0.05 MW<sub>e</sub> slipstream system with over 11,000 hours of runtime at NCCC
- 1 MW<sub>e</sub> small pilot operation at NCCC was completed in 2015. Testing successfully demonstrated optimized modules (low ∆p, low cost) with over 1,500 hours of runtime
- 1 MW<sub>e</sub> small pilot was successfully integrated with the B&W research boiler for five weeks of integrated testing with CO<sub>2</sub> recycle to the boiler in late 2016
- The integrated membrane-boiler field test experimentally validated simulated system performance
- Boiler flame was stable throughout parametric testing allowing a full battery of stream conditions and boiler efficiency measurements



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