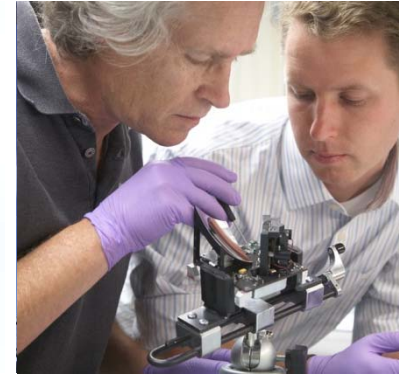


SRI International

First computer mouse



Created "Siri" for i-phone



Engineering-Scale Demonstration of the Mixed-Salt Process (MSP) for CO₂ Capture

DOE Contract: DE-FE0031588

Presented by: Indira Jayaweera, Sr. Staff Scientist and Sr. Program Manager

SRI International

333 Ravenswood Ave.

Menlo Park CA 94025



Carbon Management Technology Conference (CMTC), Houston - July 17, 2019

- SRI is an independent, leading nonprofit research organization
 - Founded by Stanford University in 1946
 - Annual R&D Projects: ~ \$500 million
- Mission : To change the world by making people safer, healthier, and more productive!

SRI Ventures

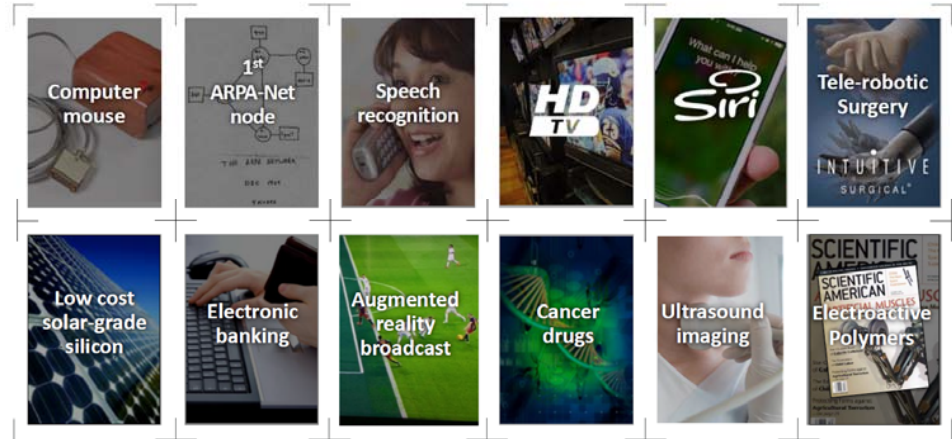
SRI Ventures is the commercialization arm of SRI International. We have created and launched more than **70 ventures** with a total market capitalization of over **\$20 billion**. Over **33%** of our companies have had successful exits.

In 2017, we launched 7 startups and they raised **over \$60 million**.

In 2018, we launched 7 successfully-funded startups

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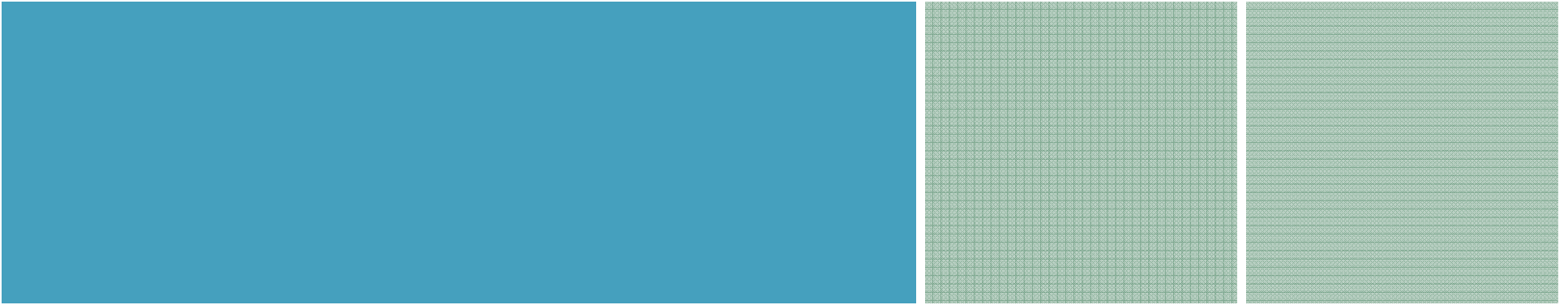
Portfolio Companies





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Project Background and Technology

Project Objectives

(DOE Contract: FE0031588)

- Perform integrated MSP testing at engineering scale for long-term periods under dynamic and continuous steady-state conditions with a real flue gas stream to address concerns relating to scale-up and integration of the technology to coal-based power plants;
- Operate the MSP with advanced heat integration to improve the process efficiencies;
- Study the solvent and water management strategies; and
- Collect critically important data for a detailed techno-economic analysis (TEA) and for further process advancements to reach the DOE's goal of \$30/tonne of CO₂ by 2030.

Key Focus:

(1) Process optimization, energy efficiency, chemical consumption and low emissions

(2) Dynamic and steady-state operations

Project Team

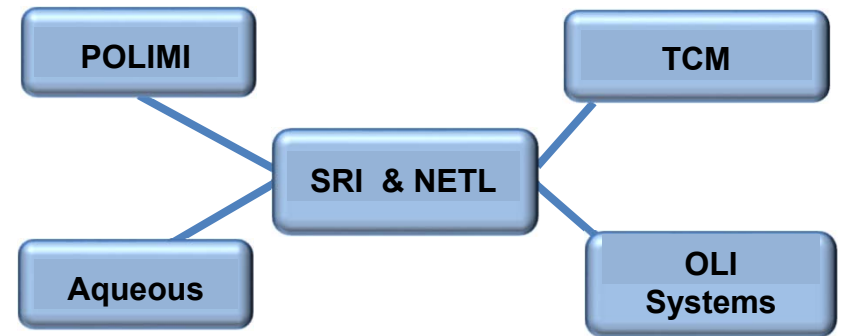
DOE Project Manager: Andrew Jones

Prime Contractor: SRI International

Project Team: US and International Partners

Project Value: ~ \$22 M

(DOE funding and TCM in-kind cost-share)



- TASK 1.0 (BP1, BP2 & BP3) - Project Management and Execution
- Task 2 (BP1) - Detailed investigation of required changes to the TCM CAP Plant to run MSP
- TASK 3.0 (BP2) - Re-commissioning of the CAP Pilot at TCM
- TASK 4.0 (BP2) - System Modification, Modeling and Initial Testing
- TASK 5.0 (BP3) - Dynamic and Steady-state Testing of MSP
- TASK 6.0 (BP3) - Process Economics, Technology Gaps and Technology Maturation
- TASK 7.0 (BP3) - Environmental, Health and Safety (EH&S) Assessment
- TASK 8.0 (BP3) - Pilot plant shutdown and Project Closure

Work Organization

SRI International

Technology provider

Technology Center Mongstad (TCM), Norway

Host site and cost-share partner

OLI Systems, USA

Process modeling

Aqueous Systems Aps, Denmark

Thermodynamic modeling

POLIMI, Italy

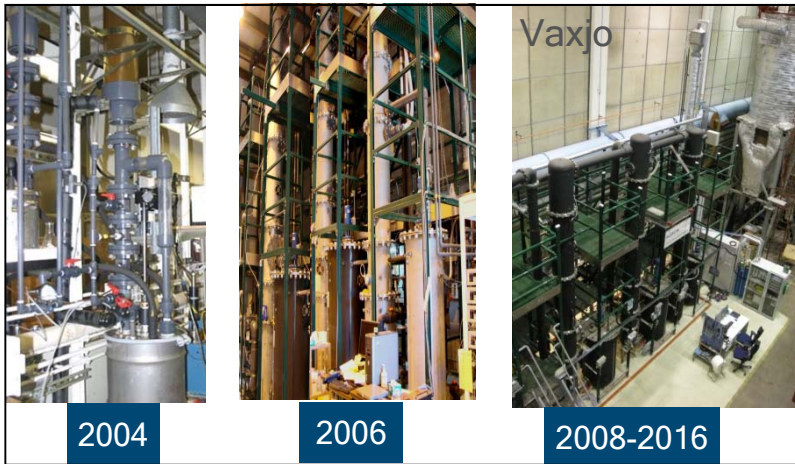
Techno-economic analysis

MSP Developments

Small bench to mini-pilot to large pilot

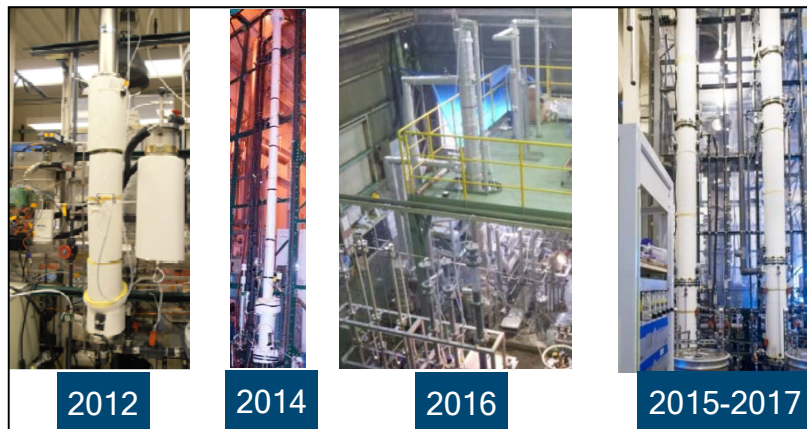
Ammonia technology development started at SRI in 2004

Chilled Ammonia Process (CAP)



CAP Validation at TCM

Mixed-Salt Process (MSP)



MSP Testing at TCM
DE-FE0031588

Step change

Mixed-Salt Process (MSP)

How it works:

Selected composition of potassium carbonate and ammonium salts

- Overall heat of reaction 35 to 60 kJ/mol (tunable)

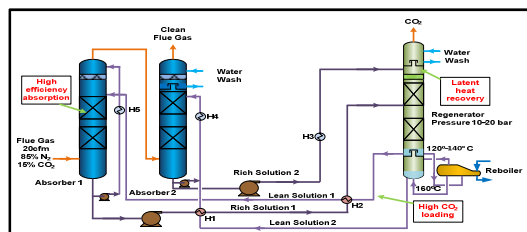
Absorber operation at 20° - 40° C at 1 atm with 30-40 wt.% mixture of salts

Regenerator operation at 120° - 160° C at 10-20 atm

- Produce high-pressure CO₂ stream

$K_2CO_3-NH_3-CO_2-H_2O$ system

High CO₂ cycling capacity



Process Highlights:

- Reduced ammonia emissions
- Enhanced efficiency
- Reduced reboiler duty
- Reduced CO₂ compression energy

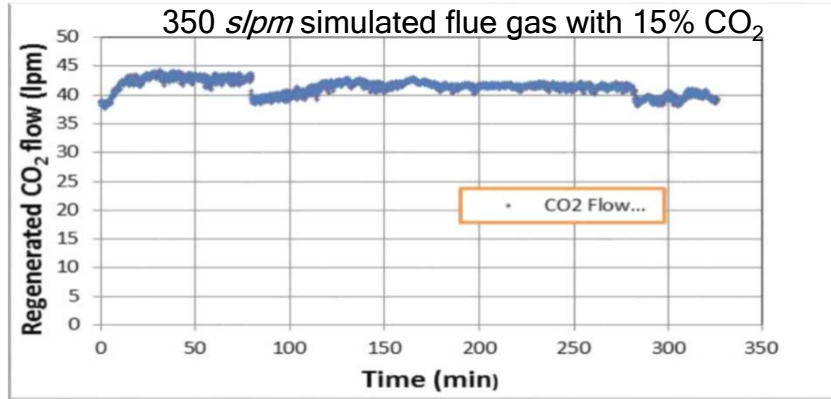
**A SIGNIFICANT PARASITIC POWER REDUCTION
COMPARED TO MEA !**



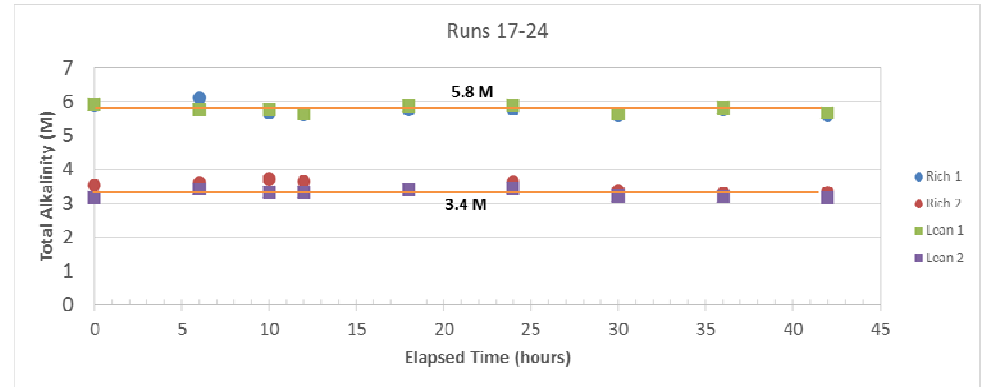
MSP Mini-pilot at SRI

Examples of Steady-State and Dynamic Testing of the Large Bench (mini-pilot)

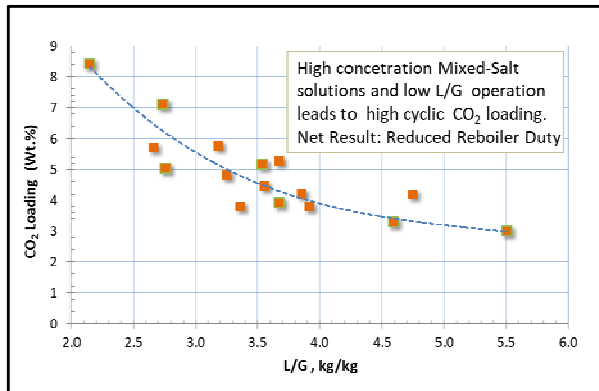
Results from FE0012959



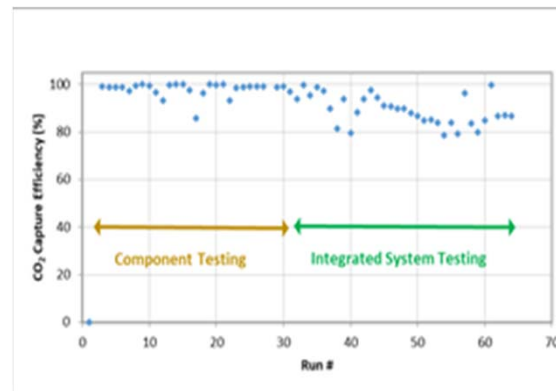
Observed 90% capture efficiency and regeneration with cyclic loading of ~0.7 mole of CO₂/mole of ammonia



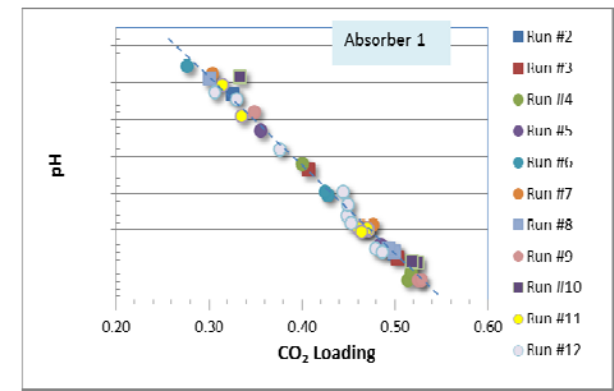
Alkalinity of rich and lean solutions circulating in the integrated system



Observed CO₂ loading as a function of L/G



CO₂ capture efficiency in parametric test runs



Observed pH as a function of CO₂ loading

Absorber: 20-35°C; Regenerator : 140°C; Reboiler: 160°C; L/G = 2 to 6 (kg/kg); Solvent composition: 5 to 8 m

MSP Summary and Benefits

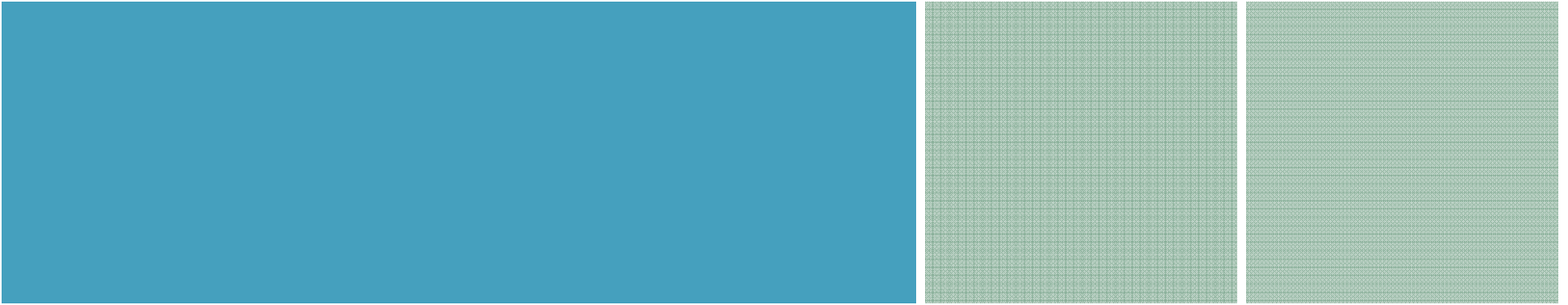
Process Summary

- Uses inexpensive, industrially available material (potassium and ammonium salts)
- No chemical degradation
- Has the potential for easy permitting in many localities
- Uses known process engineering
- Accelerated development possible



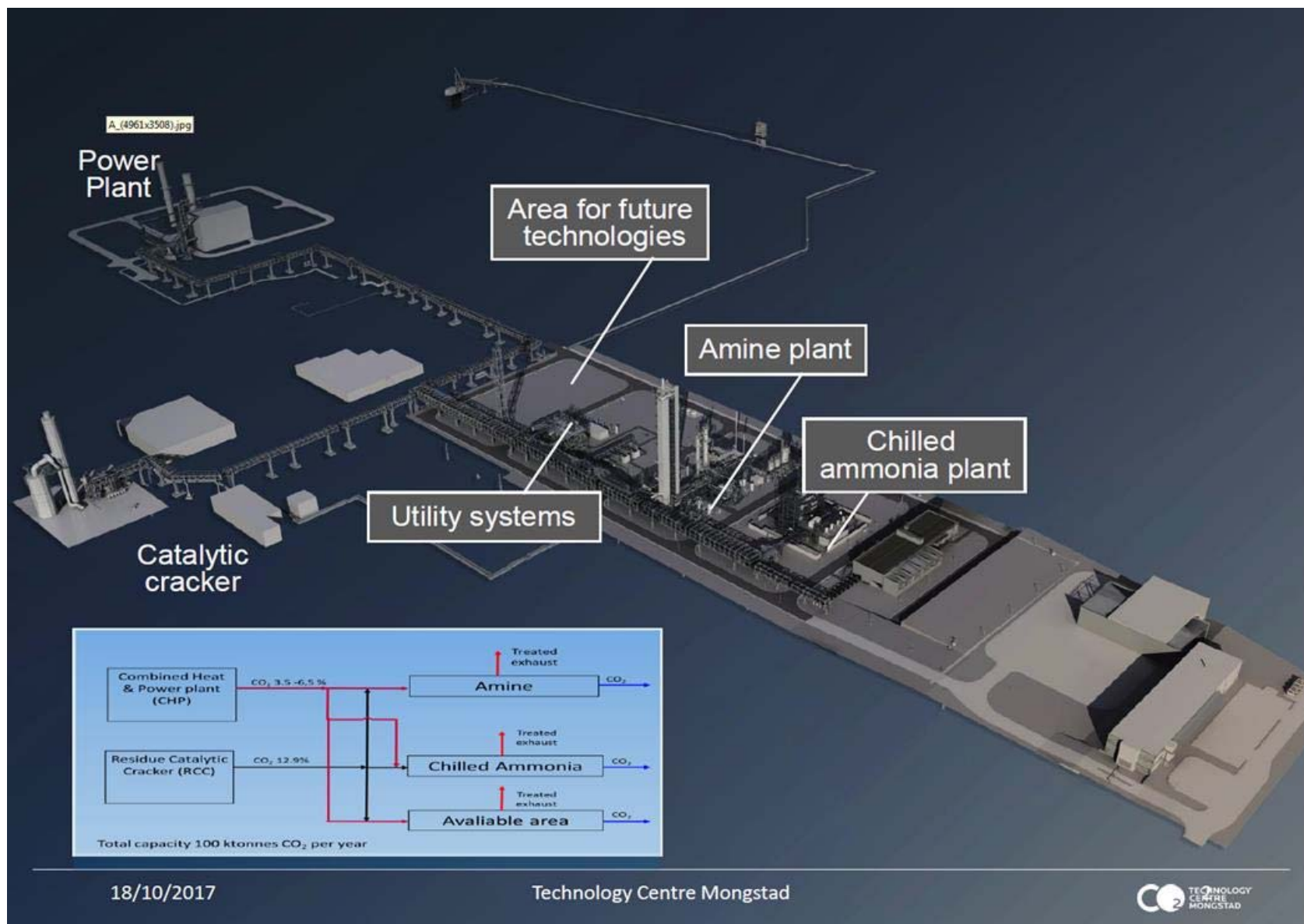
Demonstrated Benefits (By testing and/or modeling)

- Enhanced CO₂ capture efficiency
- High CO₂-loading capacity
- High-pressure release of CO₂ (10-20 bar)
- Reduced energy consumption (~ 2 MJ/kg-CO₂)
- Reduced auxiliary electricity loads



Project Start and Site Preparation

Plant View of TCM

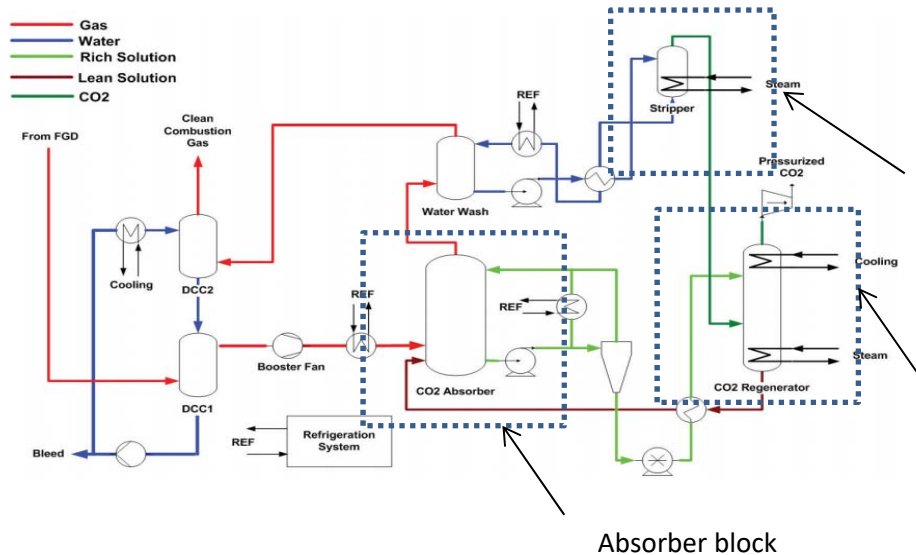


CAP Plant at Technology Center Mongstad (TCM)



Source: https://www.norskipetroleum.no/wp-content/uploads/TCM_Mongstad_foto_Helge_Hansen_Statoil_1440_480-1440x480-c-default.jpg

Existing CAP Infrastructure at TCM



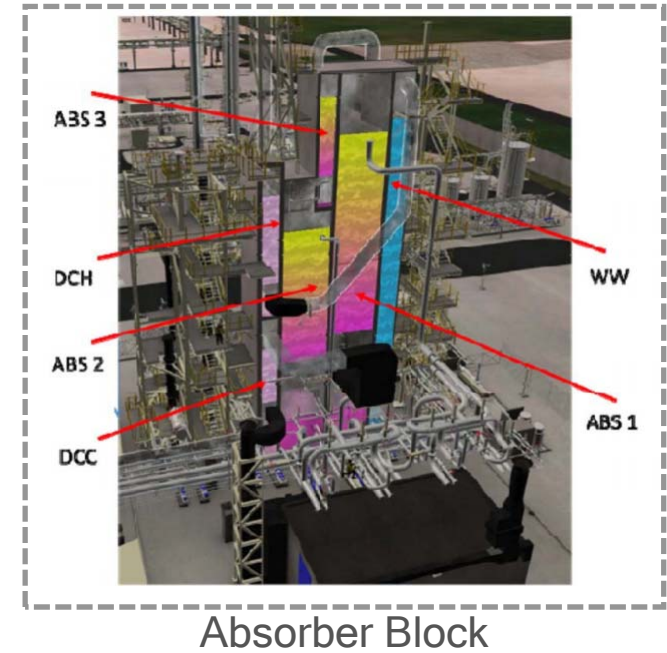
Process flow diagram of the as-built CAP system

Source: Energy Procedia 114 (2017) 5593 – 5615

Ammonia recovery block

Regenerator block

Absorber block

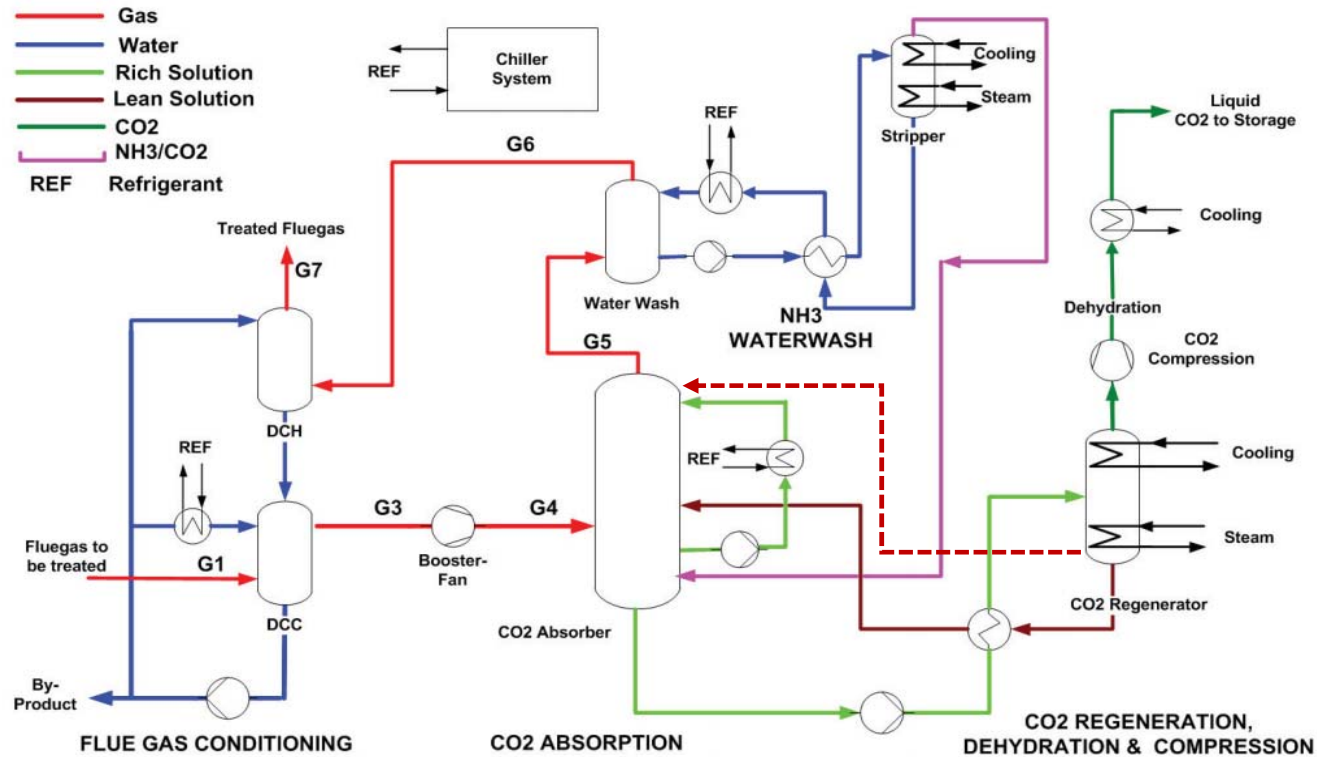


Regenerator and Ammonia Recovery Blocks

Source: Energy Procedia 51 (2014) 31 – 39

CAP System Modification

MSP testing will be in non-solid mode



Non Solid Mode Operation Flow Scheme

Key Modifications:

Absorber rearrangement (piping, valves etc.)

New lean transfer line from regenerator to absorber (piping, valves etc.)

Project Timeline

For system recommission, modification and testing

Completed or Ongoing Activities:

Contract Negotiation Phase 1 ✓

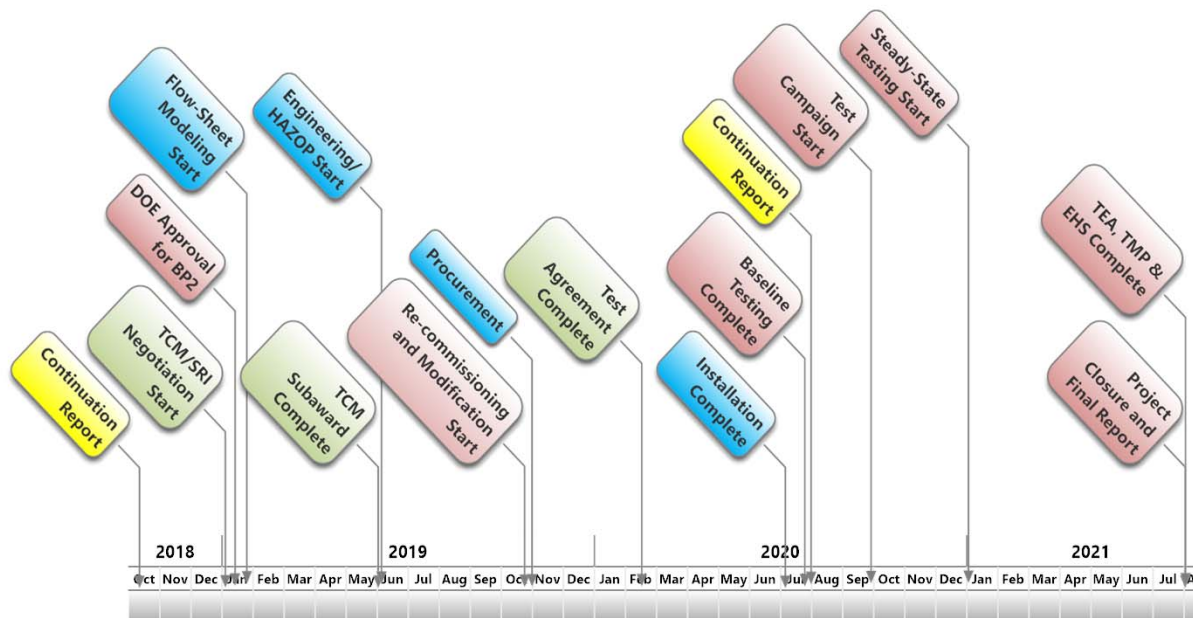
Prep work for recommission - system investigation ✓

Contract Negotiation Phase 2 ✓

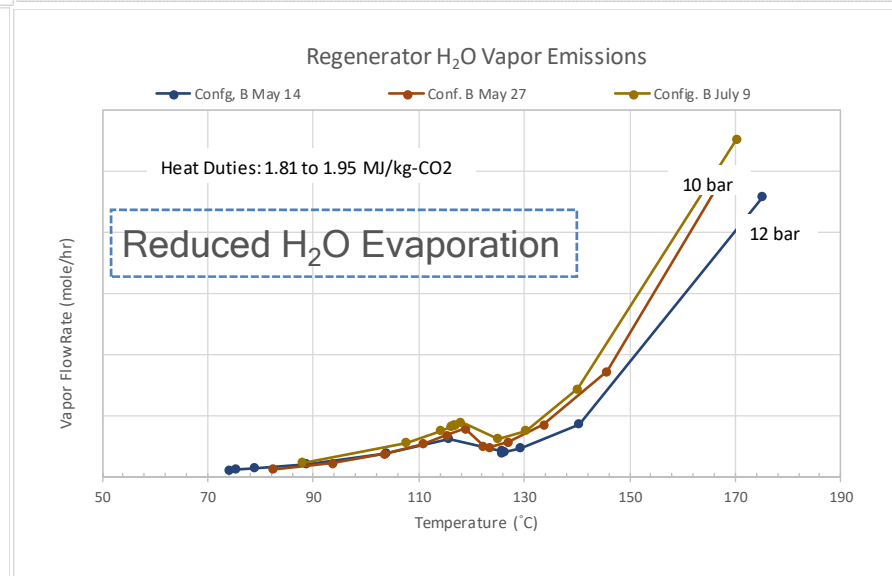
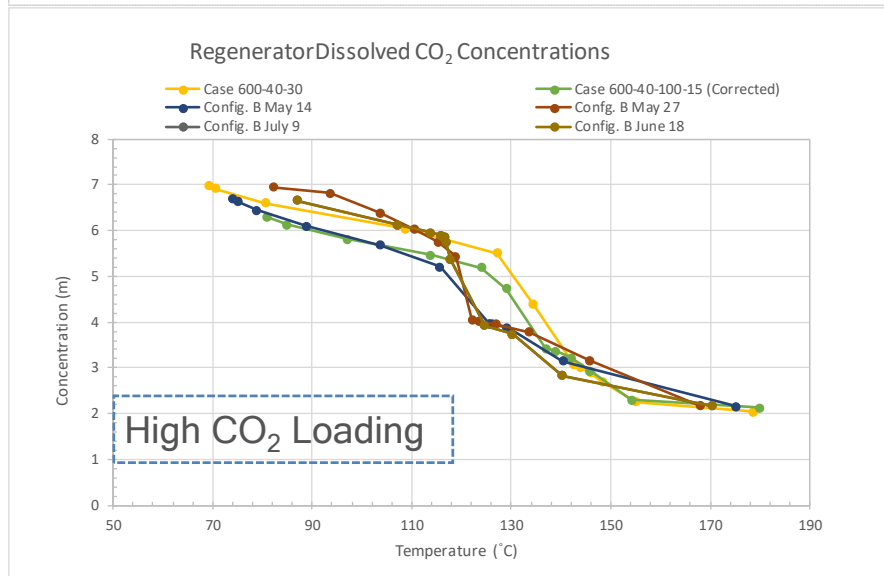
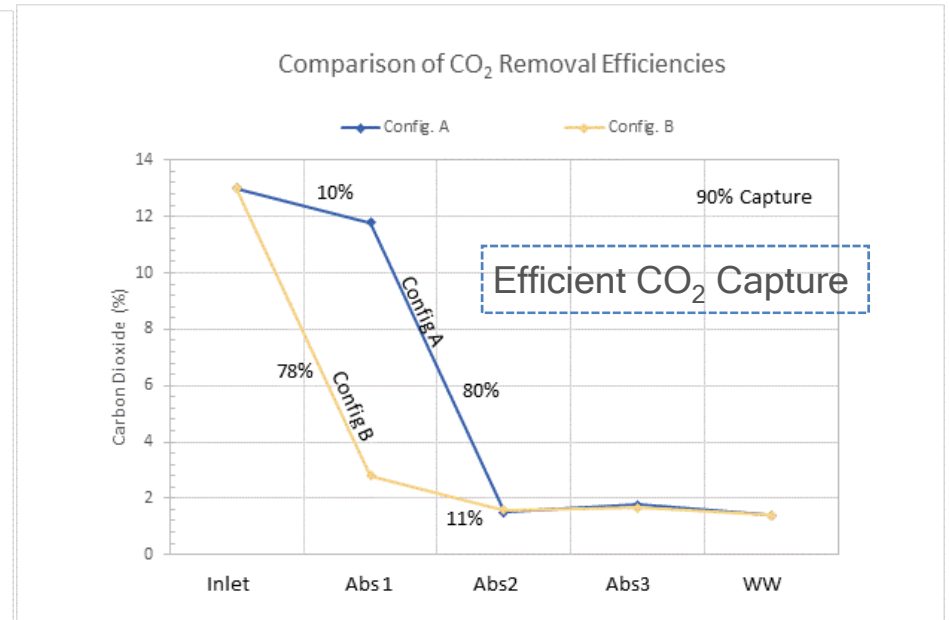
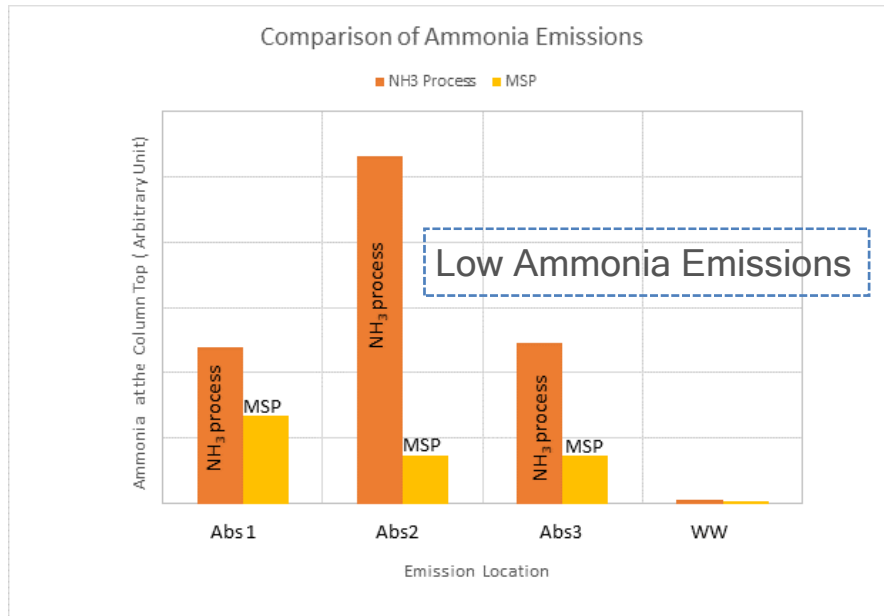
Prep Work and Engineering for Modification (in progress)

Flow-sheet modeling ✓

HAZOP (in preparation)

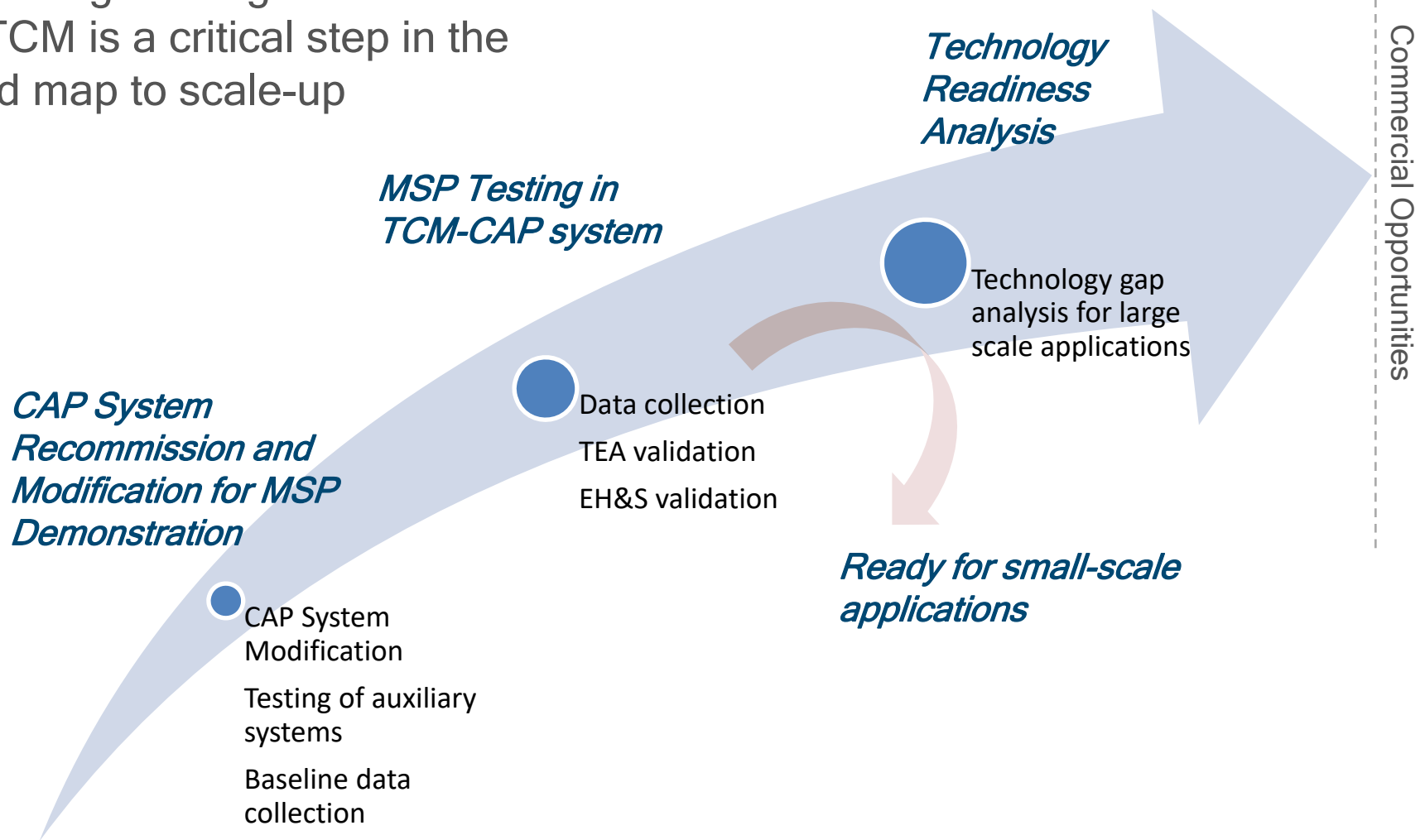


Selected Results from Flowsheet Modeling



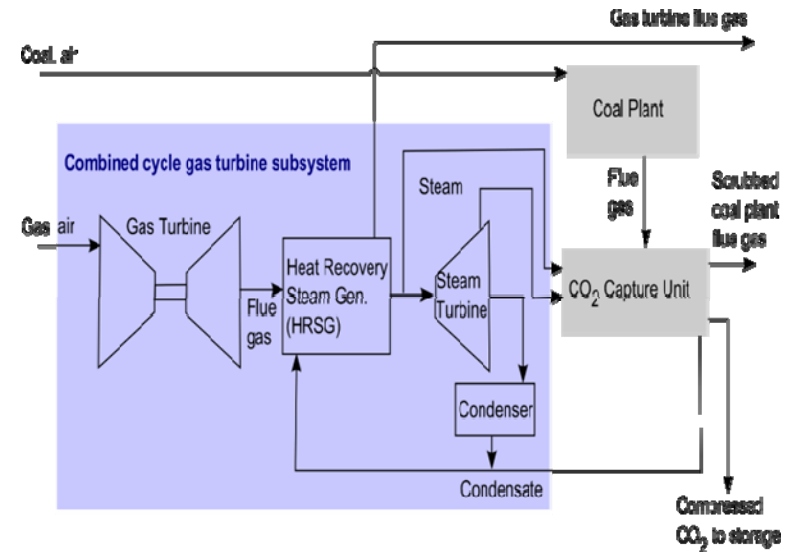
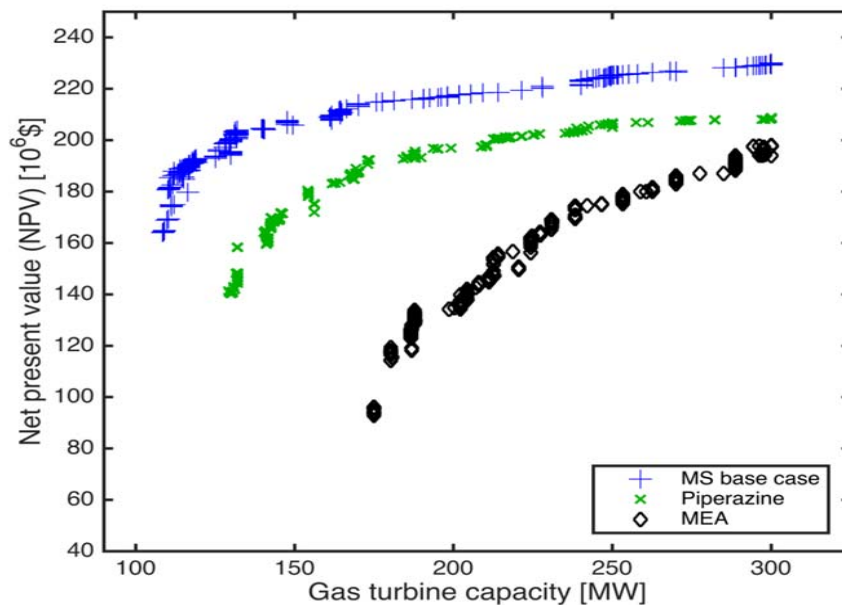
Pathway Toward Testing MSP at TCM and Beyond

MSP engineering demonstration at TCM is a critical step in the road map to scale-up

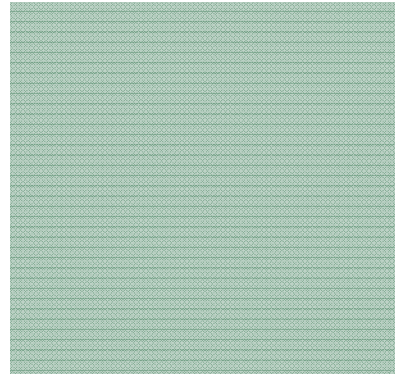
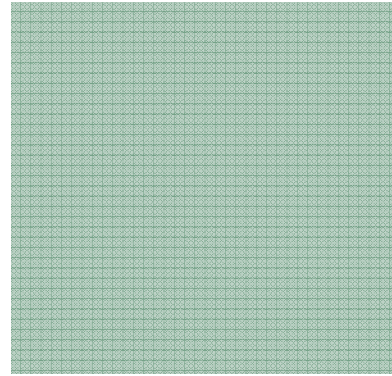


SRI has the patent coverage for MSP in US, Japan and Europe

MSP Carbon Capture Technology Integration with the Power Plant



Comparison of MSP with amine systems. Left- Modeling of auxiliary gas fired CCS for retrofits of coal-fired power stations. Right -Schematic of the CCS enabled facility



Acknowledgements

Our Past and Current Partners in CO₂ Capture Technology Development



Aqueous Solutions Aps, Inc



DTU Technical University of Denmark



IHI Corporation



Teams for Mixed-Salt Related Activities

NETL (DOE)

- Andrew Jones, Steven Mascaro, Jose Figueroa, Lynn Brickett, John Litynski and other NETL staff members

SRI Team

- Indira Jayaweera, Palitha Jayaweera, Elisabeth Perea, Regina Elmore, William Olsen, Chris Lantman, Kelli Connolly, Lisa Wottrich and Rene Harmount

Host Site

- TCM (Bjørn-Erik Haugan, Jorunn Brigsten, Kjetil Hantveit, Gerard Lombardo, Muhammad Ismail Shah and others)

Other Collaborators and Contributors

- OLI Systems (Ron Springer, Prodip Kondu and Andre Anderko)
- POLIMI (Davide Bonalumi, Stefano Lillia and Gianluca Valenti)
- Stanford University (Adam Brant and Charles Kang)
- Aqueous (Kaj Thomsen)
- BHGE (Gianluca Difederico, and Olaf Stallmann)
- IHI Corporation (Shiko Nakamura, Okuno Shinya, Yasuro Yamanaka, Kubota Nabuhiko, and others)

Thank You

SRI International

Headquarters
333 Ravenswood Avenue
Menlo Park, CA 94025
+1.650.859.2000

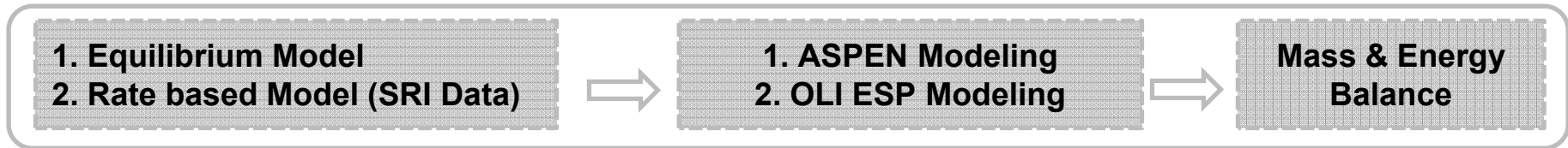
Additional U.S. and
international locations

www.sri.com

Contact:

Dr. Indira Jayaweera
Indira.jayaweera@sri.com
1-650-859-4042

Process Economic Data



Cost of Electricity (COE) Comparison

	NETL, Case 12 (2013)	NETL, Case 12B (2015)	SRI
Component, \$/MWh	Econamine	Cansolv	MSP
Capital	66.4	72.2	57.1
Fixed	14.5	15.4	15.4
Variable	12.1	14.7	12.6
Fuel	35.3	30.9	32.3
Total (Excluding T&S)	128.2	133.2	117.4
CO ₂ T&S	11.0	9.6	10.0
Total (including T&S)	139.2	142.8	127.3

Total Auxiliary Consumption [MWe]	112.8	91.0	72.0
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- MSP has a COE almost 11% lower than CANSOLV
- The auxiliary consumption of the MSP technology are the lowest, mainly due to the lower CO₂ compression energy consumption in MSP compared to amine technologies.