Fluidization XVI

Flow Characteristics in the Downward FCC Feed Injection Scheme

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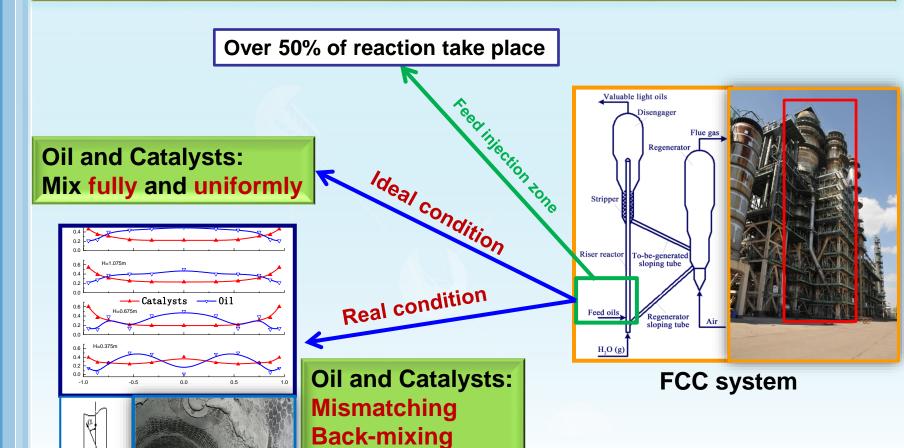
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1. INTRODUCTION



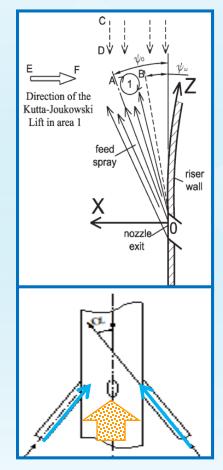
Fluid catalytic cracking (FCC) is an important primary conversion process in modern oil refining industry, providing a variety of high value products such as gasoline, middle distillate and light olefins.



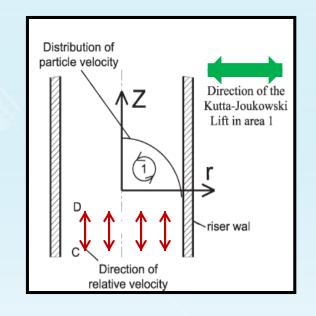
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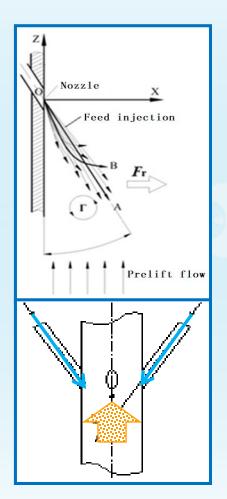


1. INTRODUCTION



Traditional feed injection scheme





Downward feed injection scheme

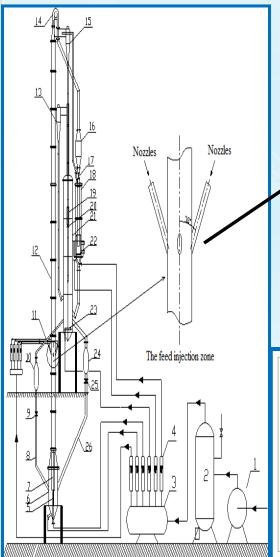


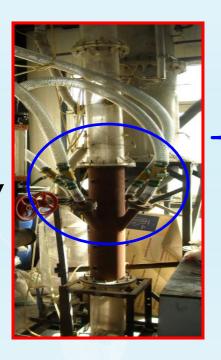
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2. EXPERIMENTS





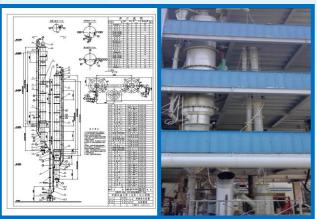


Optical fiber probe

Particle concentration and velocity

Helium-tracer

Jet concentration, Residence time distribution



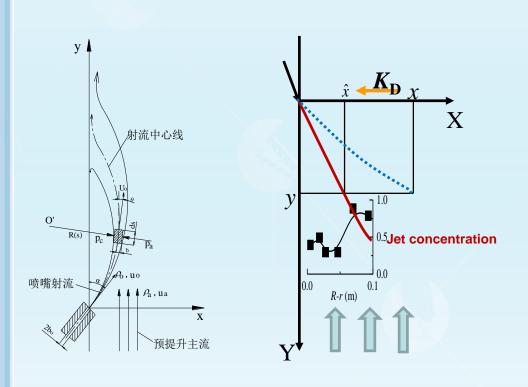


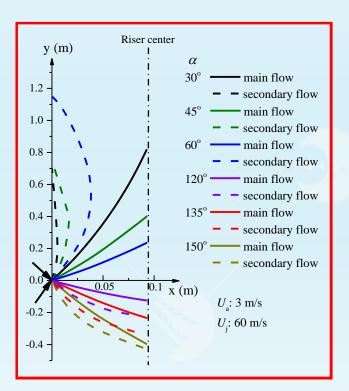
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3.1 Trajectory of feed injection



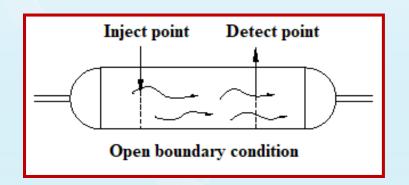


$$\hat{x} = \frac{1}{K_{D}} \cdot \frac{-C \pm (C^{2} + 2ADy - BDy^{2})^{0.5}}{D} = \frac{1}{K_{D}} x$$

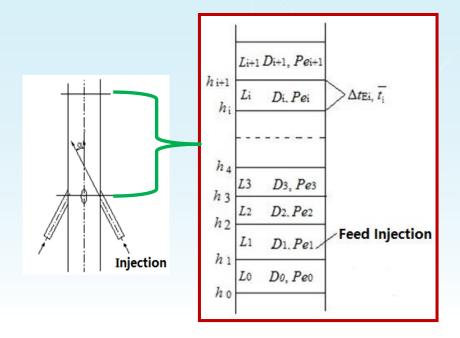




3.2 Diffusion of feed injection



$$\theta = \frac{t_{\rm m}}{\bar{t}} = 1 + \frac{1}{Pe_{\rm a}} \left(\frac{D_{\rm a1}}{D_{\rm a}} + \frac{D_{\rm a2}}{D_{\rm a}} \right)$$

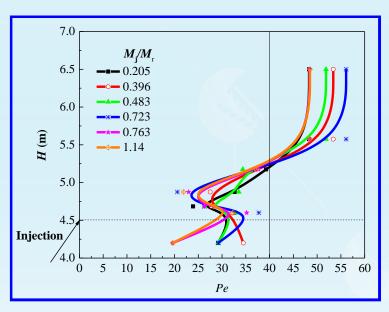


$$\begin{split} \theta_1 &= \frac{\Delta t_{\text{m1}}}{\overline{t_1}} = 1 + \frac{1}{u_1 L_1} \left(\frac{u_0 L_0}{P e_0} + \frac{u_2 L_2}{P e_2} \right) \\ \theta_2 &= \frac{\Delta t_{\text{m2}}}{\overline{t_2}} = 1 + \frac{1}{u_2 L_2} \left(\frac{u_1 L_1}{P e_1} + \frac{u_3 L_3}{P e_3} \right) \\ &\dots \\ \theta_i &= \frac{\Delta t_i}{\overline{t_i}} = 1 + \frac{1}{u_i L_i} \left(\frac{u_{i-1} L_{i-1}}{P e_{i-1}} + \frac{u_{i+1} L_{i+1}}{P e_{i+1}} \right) \end{split}$$



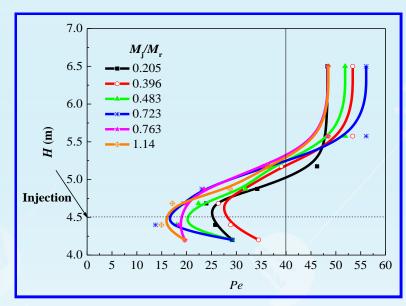
3.2 Diffusion of feed injection

Distribution of Peclet number



Upward nozzles

Pe:↑, ↓a little, then to plug flow



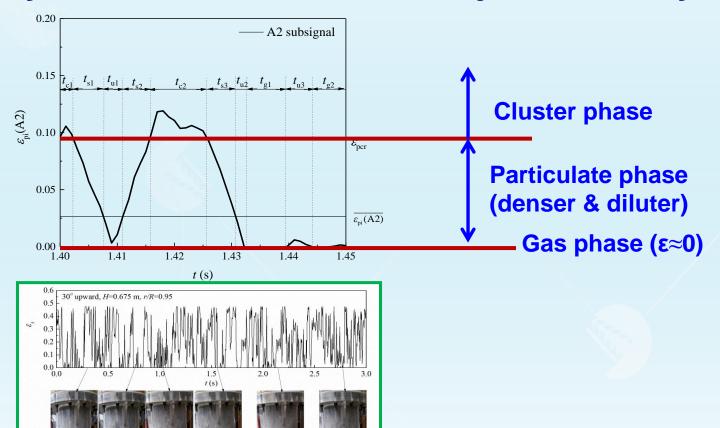
Downward nozzles

Pe: to a low value then to plug flow

Promote to mixing between feed oil with catalysts









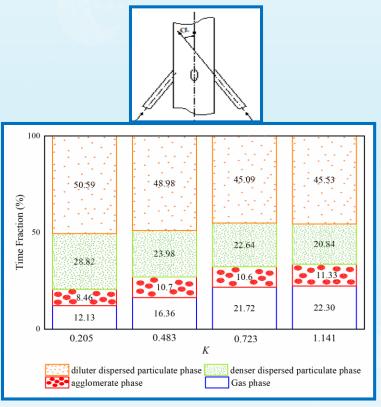
2.0

2.5



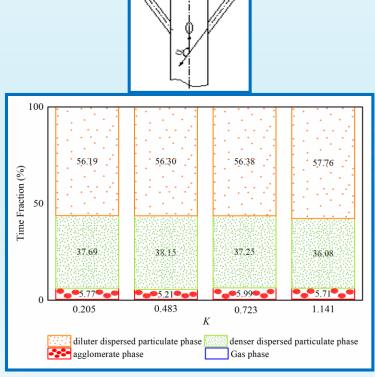


3.3 Dynamic behaviors between jet and catalysts



Upward nozzles

Cluster phase: high Gas phase: quite high



Downward nozzles

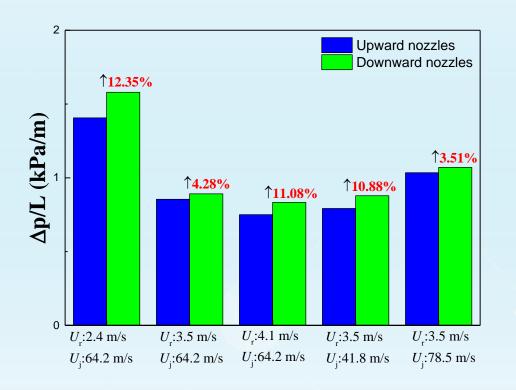
Cluster and gas phases: low Particulate phase: high







3.4 Pressure drop



Downward nozzles:

No significant increase in pressure drop is seen!

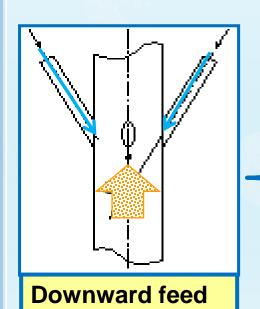


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4. CONCLUSIONS





injection scheme

Reduce back-mixing near the riser wall

Flow pattern:

complete mixed flow → plug flow, quickly

Dynamic mixing:

Reduce cluster and gas phases Increase particulate phase

Pressure drop:

No significant increase

Great potential of application



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Thank you!



